

7.3 Laminar Boundary Layer Similarity Solutions

Laminar Boundary Layer: $Re_{crit} = 91,000$; $Re_{trans} = 5 \times 10^5 - 3 \times 10^6$.

Similarity solutions (2D, steady, incompressible): method of reducing PDE to ODE by appropriate similarity transformation; also, because of transformation at least one coordinate lacks origin such that the solution collapses to same form at all length or time scales.

$$\begin{aligned} u_x + v_y &= 0 \\ uu_x + vu_y &= UU_x + vu_{yy} \end{aligned}$$

BCs: $u(x, 0) = v(x, 0) = 0$ no slip
 $u(x, \infty) = U(x)$ matching outer flow
 + inlet condition

For Similarity $\frac{u(x,y)}{U(x)} = F\left(\frac{y}{g(x)}\right)$ expect $g(x)$ related to $\delta(x)$

Or in terms of stream function $\Psi : u = \psi_y \quad v = -\psi_x$

For similarity $\psi = U(x)g(x)f(\eta) \quad \eta = y/g(x)$

$$u = \psi_y = Uf' \quad v = -\psi_x = -(U_xgf + Ug_xf - Ug_x\eta f')$$

BC:

$$u(x,0) = 0 \Rightarrow U(x)f'(0) = 0 \Rightarrow f'(0) = 0$$

$$v(x,0) = 0 \Rightarrow U_x(x)g(x)f(0) + U(x)g_x(x)f(0)$$

$$-U(x)g_x(x) \times 0 \times f'(0) = 0$$

$$\Rightarrow (U_x(x)g(x) + U(x)g_x(x))f(0) = 0$$

$$\Rightarrow f(0) = 0$$

$$u(x, \infty) = U(x) \Rightarrow U(x)f'(\infty) = U(x) \Rightarrow f'(\infty) = 1$$

Write boundary layer equations in terms of ψ

$$\psi_y \psi_{yx} - \psi_x \psi_{yy} = UU_x + \nu \psi_{yyy}$$

Substitute

$$\psi_{yy} = Uf'' / g$$

$$\psi_{yyy} = Uf''' / g^2$$

$$\psi_{xy} = U_x f' - Uf'' \eta g_x / g$$

Assemble them together:

$$\begin{aligned} (Uf') \left(U_x f' - Uf'' \frac{g_x}{g} \right) - (U_x g f + U g_x f - U g_x \eta f') (Uf'' / g) \\ = UU_x + \nu (Uf''' / g^2) \end{aligned}$$

$$UU_x f'^2 - UU_x f f'' - (U^2 g_x / g) f f'' = UU_x + \nu \frac{U}{g^2} f'''$$

$$UU_x f'^2 - \frac{U}{g} (Ug)_x f f'' = UU_x + \nu \frac{U}{g^2} f'''$$

$$f''' + \underbrace{\frac{g}{\nu} (Ug)_x}_{C_1} f f'' + \underbrace{\frac{g^2}{\nu} U_x}_{C_2} (1 - f'^2) = 0$$

Where for similarity C_1 and C_2 are constant or function η only

- i.e. for a chosen pair of C_1 and $C_2 \rightarrow U(x), g(x)$ can be found, i.e., potential flow is NOT known a priori.
- Then solution of $f''' + C_1 f f'' + C_2 (1 - f'^2) = 0$ gives $f(\eta) \rightarrow u(x, y), \tau_w = \mu \frac{\partial u}{\partial y} \Big|_w = \frac{\mu U f''(0)}{g}, \delta, \delta^*, \theta, H, C_f, C_D$

The Blasius Solution for Flat-Plate Flow

$$U = \text{constant} \rightarrow U_x = 0 \rightarrow C_2 = 0$$

$$\text{Then } C_1 = \frac{U}{\nu} g g_x \neq \text{function}(x)$$

$$\frac{d}{dx}(g^2) = \frac{2C_1 \nu}{U} \implies g(x) = [2C_1 \nu x / U]^{1/2}$$

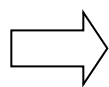
$$\text{Let } C_1 = 1, \text{ then } g(x) = \sqrt{\frac{2\nu x}{U}} \implies \eta = y \sqrt{\frac{U}{2\nu x}} = \frac{y}{\sqrt{\frac{2\nu x}{U}}} \propto \frac{y}{\delta}$$

$$\text{Note } \frac{\delta}{x} = \frac{5}{\sqrt{Re_x}}, \text{ i.e., } \delta = \frac{5x}{\sqrt{\frac{Ux}{\nu}}} = 5 \sqrt{\frac{\nu x}{U}}$$

$$\psi = U [2\nu x / U]^{1/2} f \left(y \sqrt{\frac{U}{2\nu x}} \right) = \sqrt{2\nu U x} f(\eta)$$

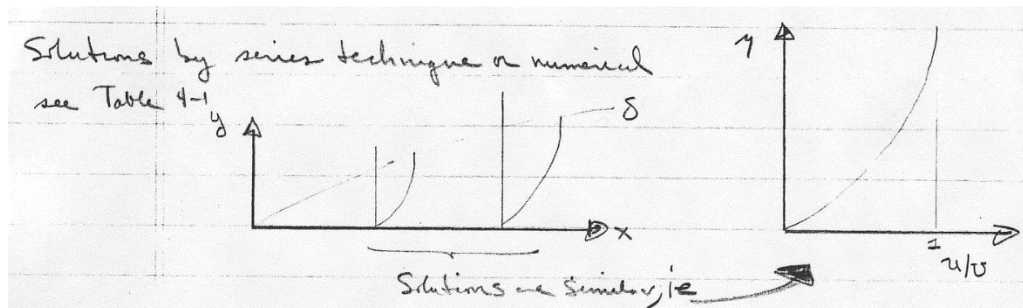
$$u = \psi_y = U f'$$

$$v = -\psi_x = U g_x (\eta f' - f) = [U\nu / 2x]^{1/2} (\eta f' - f) = \frac{U(\eta f' - f)}{\sqrt{2Re_x}}$$



$f''' + ff'' = 0$ $f(0) = f'(0) = 0, f'(\infty) = 1$	Blasius equations for Flat Plate Boundary Layer
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Solutions by series or numerical methods



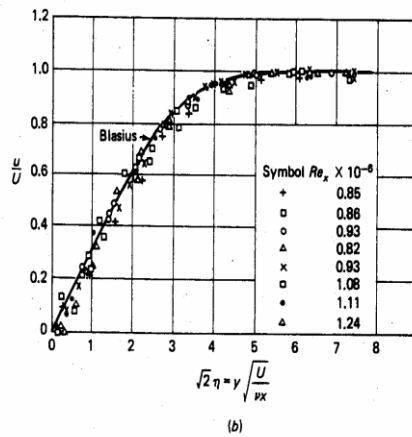
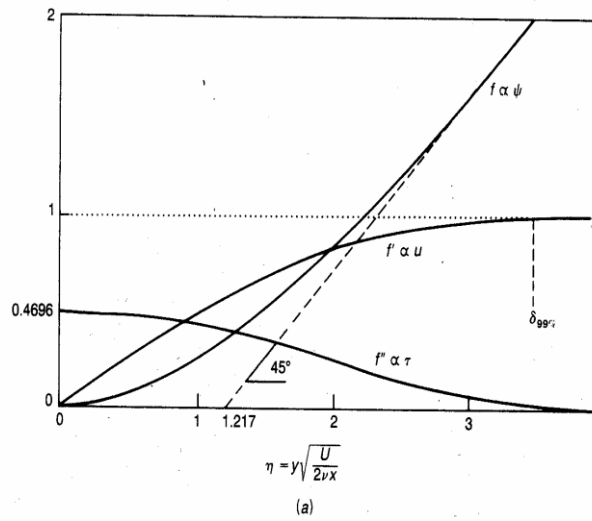


FIGURE 4-6 The Blasius solution for the flat-plate boundary layer: (a) numerical solution of Eq. (4-45); (b) comparison of $f' = u/U$ with experiments by Liepmann (1943).

Fig. 7.10. Local coefficient of skin friction on a flat plate at zero incidence in incompressible flow, determined from direct measurement of shearing stress by Liepmann and Dhawan [6, 18]
 Theory: laminar from eqn. (7.32); turbulent from eqn. (21.12)

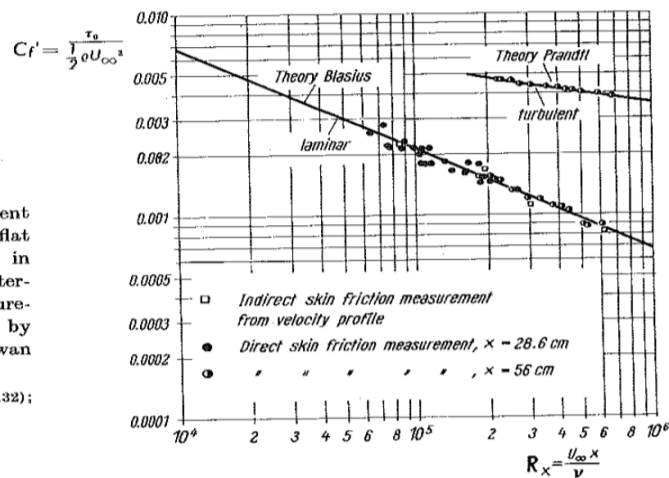


TABLE 4-3

Highly resolved numerical solution of the Blasius equation for flow over a flat plate, Eq. (4-60)

η	$\eta/\eta_{99\%}$	$f(\eta)$	$f'(\eta)$	$f''(\eta)$	$f'''(\eta)$
0.0	0.00000	0.00000	0.00000	0.46960	0.00000
0.0	0.05761	0.00939	0.09391	0.46931	-0.00441
0.4	0.11521	0.03755	0.18761	0.46725	-0.01755
0.6	0.17282	0.08439	0.28058	0.46173	-0.03896
0.8	0.23042	0.14967	0.37196	0.45119	-0.06753
1.0	0.28803	0.23299	0.46063	0.43438	-0.10121
1.2	0.34563	0.33366	0.54525	0.41057	-0.13699
1.4	0.40324	0.45072	0.62439	0.37969	-0.17114
1.6	0.46084	0.58296	0.69670	0.34249	-0.19966
1.8	0.51845	0.72887	0.76106	0.30045	-0.21899
2.0	0.57606	0.88680	0.81669	0.25567	-0.22673
2.2	0.63366	1.05495	0.86330	0.21058	-0.22215
2.4	0.69127	1.23153	0.90107	0.16756	-0.20636
2.6	0.74887	1.41482	0.93060	0.12861	-0.18196
2.8	0.80648	1.60328	0.95288	0.09511	-0.15249
3.0	0.86408	1.79557	0.96905	0.06771	-0.12158
3.2	0.92169	1.99058	0.98036	0.04637	-0.09230
3.3	0.95049	2.08883	0.98456	0.03781	-0.07899
3.4	0.97929	2.18747	0.98797	0.03054	-0.06679
3.47*	1.00000	2.25856	0.99000	0.02603	-0.05878
3.5	1.00810	2.28641	0.99071	0.02441	-0.05582
3.6	1.03690	2.38559	0.99289	0.01933	-0.04611
3.8	1.09451	2.58450	0.99594	0.01176	-0.03039
4.0	1.15211	2.78389	0.99777	0.00687	-0.01914
4.2	1.20972	2.98356	0.99882	0.00386	-0.01152
4.4	1.26732	3.18338	0.99940	0.00208	-0.00663
4.6	1.32493	3.38330	0.99970	0.00108	-0.00366
4.8	1.38253	3.58325	0.99986	0.00054	-0.00193
5.0	1.44014	3.78323	0.99994	0.00026	-0.00098
5.2	1.49774	3.98323	0.99997	0.00012	-0.00047
5.4	1.55535	4.18322	0.99999	0.00005	-0.00022
5.6	1.61296	4.38322	1.00000	0.00002	-0.00010
5.8	1.67056	4.58322	1.00000	0.00001	-0.00004
6.0	1.72817	4.78322	1.00000	0.00000	-0.00002

*Actual value to 16 significant digits: $\eta_\delta = 3.471886880405967$.

$$\frac{u}{U} = 0.99 \text{ when } \eta = 3.5 \rightarrow \frac{\delta}{x} = \frac{5}{\sqrt{Re_x}} \quad Re_x = \frac{Ux}{\nu}$$

$$\delta^* = \int_0^\infty \left(1 - \frac{u}{U}\right) dy = \int_0^\infty (1 - f') d\eta \sqrt{\frac{2\nu x}{U}} \rightarrow \frac{\delta^*}{x} = \frac{1.7208}{\sqrt{Re_x}}$$

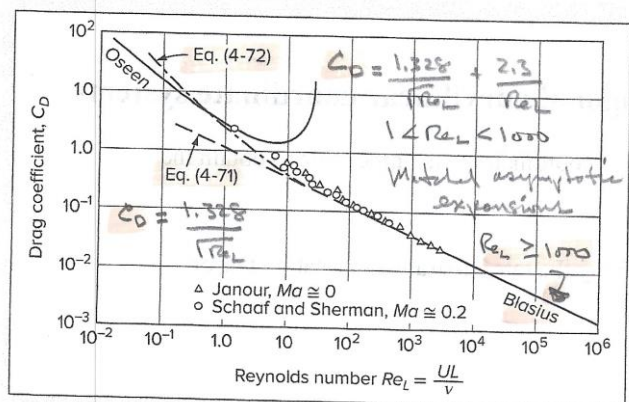
$$\theta = \int_0^\infty \left(1 - \frac{u}{U}\right) \frac{u}{U} dy = \int_0^\infty (1 - f') f' \sqrt{\frac{2\nu x}{U}} d\eta \rightarrow \frac{\theta}{x} = \frac{0.664}{\sqrt{Re_x}}$$

$$\frac{\delta^*}{\theta} = H = \text{shape parameter } 2.59$$

$$\tau_w = \mu \left. \frac{\partial u}{\partial y} \right|_w = \frac{\mu U f''(0)}{\sqrt{\frac{2\nu x}{U}}} \rightarrow C_f = \frac{\tau_w}{\frac{1}{2}\rho U^2} = \frac{0.664}{\sqrt{Re_x}} = \frac{\theta}{x}$$

$$C_D = \frac{D}{\frac{1}{2}\rho U^2 L} = \int_0^L C_f \frac{dx}{L} = \frac{1.328}{\sqrt{Re_L}} \quad Re_L = \frac{UL}{\nu}$$

$$\frac{v}{U} = \frac{\eta f' - f}{\sqrt{2Re_x}} \ll 1 \quad \text{for } Re_x \gg 1$$



Stokes flow: Oseen
 Improvement, i.e.,
 linearized
 convection
 $C_D = \frac{4\pi}{Re_L [1 - \Gamma + \ln(16/Re_L)]}$
 $\Gamma = .577216 = \text{Euler constant}$
 $Re_L \ll 1$

FIGURE 4-11
 Theoretical and experimental drag of a flat plate.

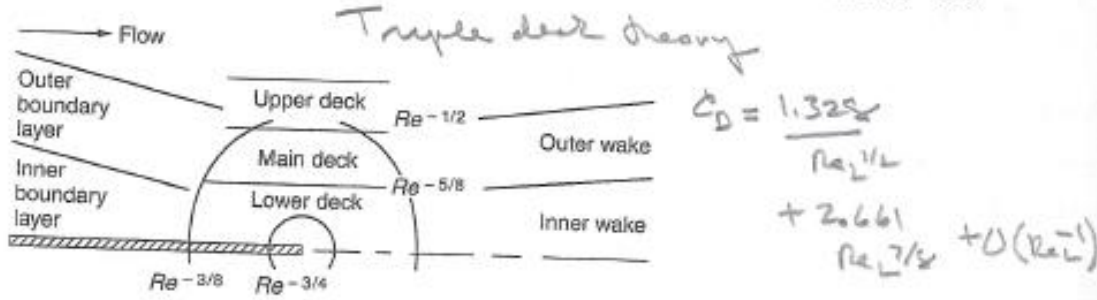
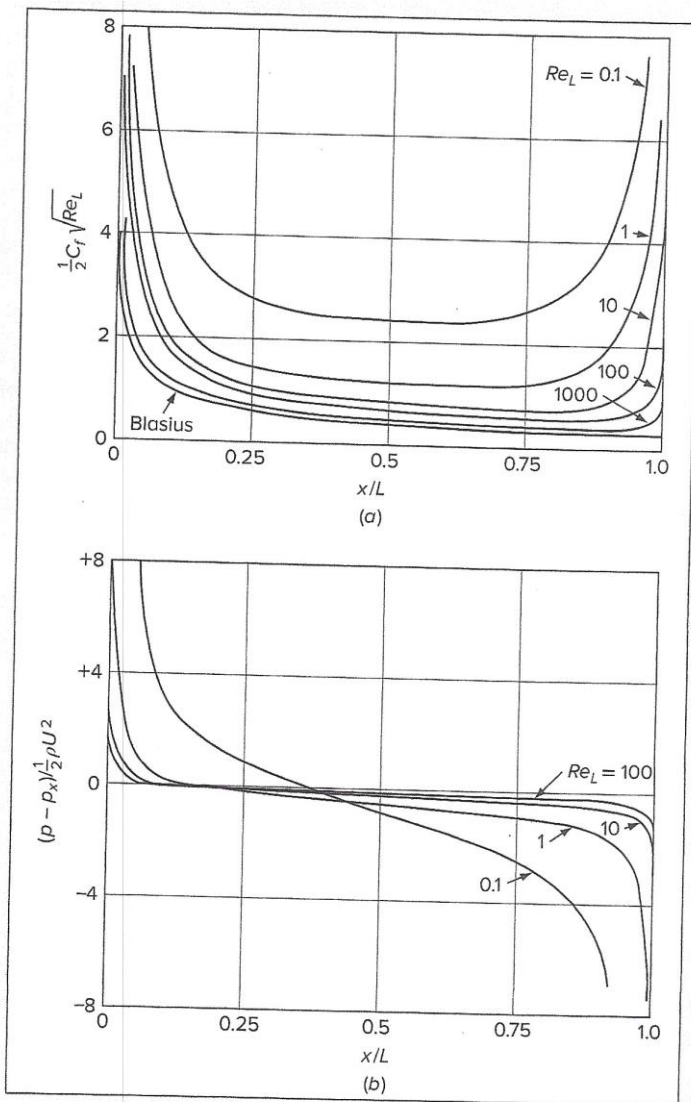


FIGURE 4-40 Sketch of the triple-deck region at the trailing edge of a flat plate, merging into two-layer upstream and downstream regions. [After Stewartson (1969) and Messiter (1970).]



WS CFD - $1 < Re_L < 1000$
 low Re large LE & TE effects
 BL approximation $Re_L \geq 1000$

FIGURE 4-12 Numerical solution of the full Navier-Stokes equations for flat-plate flow at moderate Reynolds numbers: (a) local friction coefficient; (b) local surface pressure. [After Dennis and Dunwoody (1966).]

Falkner-Skan Wedge Flows

$$\left. \begin{aligned}
 f''' + C_1 f f'' + C_2 (1 - f'^2) &= 0 & f &= f(\eta) \\
 f(0) = f'(0) &= 0, & \eta &= y/g(x) \\
 f'(\infty) &= 1 & u/U &= f'(\eta) \\
 C_1 = \frac{g}{\nu} (Ug)_x & & C_2 = \frac{g^2}{\nu} U_x & \text{(Blasius Solution: } C_2=0, C_1=1)
 \end{aligned} \right\} \text{Similarity form of BL equations}$$

Consider $(Ug^2)_x = 2Ug g_x + g^2 U_x$

$$\begin{aligned}
 &= 2Ug g_x + 2g^2 U_x - g^2 U_x = 2g(Ug_x + gU_x) - g^2 U_x \\
 &= 2g(Ug)_x - g^2 U_x \\
 &= 2\nu C_1 - \nu C_2
 \end{aligned}$$

Hence $(Ug^2)_x = \nu(2C_1 - C_2)$

Choose $C_1=1$ and let $C_2 = C$

Integrate $Ug^2 = \nu(2 - C)x$ note $g^2 = \nu C/U_x$

Combine $\frac{U\nu C}{U_x} = \nu(2 - C)x$

Rearrange $\frac{dU}{U} = \frac{C}{2-C} \frac{1}{x}$

Integrate $\ln U = \frac{C}{2-C} \ln x + \ln k$ where $\ln k = \text{constant}$

$$\ln U = \ln x^{\frac{C}{2-C}} + \ln k = \ln kx^{\frac{C}{2-C}}$$

$$U(x) = kx^{C/(2-C)}$$

$$g(x) = \left[\frac{vC}{U_x} \right]^{\frac{1}{2}} \text{ note } U_x = k \frac{C}{2-C} x^{\left(\frac{C}{2-C}-1\right)} = k \frac{C}{2-C} x^{\left(\frac{-2(1-C)}{2-C}\right)}$$

$$g(x) = \left[\frac{vC}{k \frac{C}{2-C} x^{\left(\frac{-2(1-C)}{2-C}\right)}} \right]^{\frac{1}{2}} = \left[\frac{v(2-C)}{k} x^{\left(\frac{-2(1-C)}{2-C}\right)} \right]^{\frac{1}{2}} = \sqrt{\frac{v(2-C)}{k}} x^{\frac{1-C}{2-C}}$$

using $a^{1/2}b^{1/2}=(ab)^{1/2}$ and $(a^m)^n=a^{mn}$

Alternatively, $U_x = \frac{C}{2-C} kx^{(C/(2-C))} x^{-1} = \frac{C}{2-C} Ux^{-1}$

Such that $g(x) = \left[\frac{vC}{\frac{C}{2-C} Ux^{-1}} \right]^{\frac{1}{2}} = \left[\frac{v(2-C)x}{U} \right]^{\frac{1}{2}}$

Change constant: $C = \beta = \frac{2m}{m+1}$ and $m = \frac{\beta}{2-\beta}$

$$U(x) = kx^m$$

$$\eta = \frac{y}{g} = y \sqrt{\frac{m+1}{2} \frac{U}{vx}}$$

$$f''' + ff'' + \beta(1 - f'^2) = 0$$

$$f(0) = f'(\infty) = 0 \text{ and } f'(0) = 1$$

Note:

$$2m/(m+1) = \frac{2\beta}{2-\beta} / \left(\frac{\beta}{2-\beta} + 1 \right) = \frac{2\beta}{2-\beta} / \left(\frac{2}{2-\beta} \right) = \beta$$

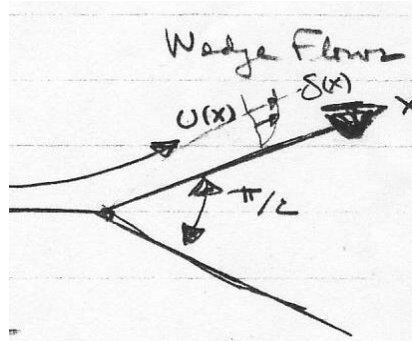
$$2-C = 2 - 2m/(m+1) = 2/(m+1)$$

$$g(x) = \left[\frac{v(2-C)x}{U} \right]^{\frac{1}{2}} = \left[\frac{v2x}{U(m+1)} \right]^{\frac{1}{2}}, \text{ i.e., } g(x)^{-1} = \left[\frac{m+1}{2} \frac{U}{vx} \right]^{\frac{1}{2}}$$

Numerical solutions for $-0.19884 \leq \beta \leq 1.0$.

↑
Separation ($\tau_w = 0$)

$$U(x) = kx^m$$



Solutions show many commonly observed characteristics of BL flow:

- The parameter β is a measure of the pressure gradient, dp/dx . For $\beta > 0$, $dp/dx < 0$ and the pressure gradient is favorable. For $\beta < 0$, the $dp/dx > 0$ and the pressure gradient is adverse.
- Negative β solutions drop away from Blasius profiles as separation approached.
- Positive β solutions squeeze closer to wall due to flow acceleration.
- Accelerated flow: τ_{\max} near wall.
- Decelerated flow: τ_{\max} moves toward $\delta/2$

Inviscid flow past wedges & corners

$\psi(x) = Kx^m$ exact solution potential flow
 past wedge or corner shapes

Plane polar coordinates $\nabla^2 \psi = 0$, $\nabla \times \mathbf{v} = 0$

$$\frac{1}{r^2} \left(r^2 v_r \right) + \frac{1}{r^2} \chi_{\theta\theta} = 0 \quad \Rightarrow v_r = \frac{1}{r} \chi_\theta \quad v_\theta = -\chi_r$$

$$\chi(r, \theta) = C r^{m+1} \sin[(m+1)\theta] \quad \beta = \frac{2m}{m+1}$$

$$m = \beta / (2 - \beta)$$

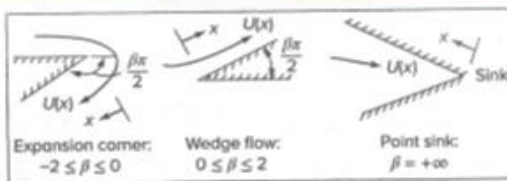


FIGURE 4-15
 Some examples of Falkner-Skan potential flows.

This expression yields certain radial streamlines that can be interpreted as the "walls" of a wedge or a corner, as shown in Fig. 4-15, depending on the value of $\beta = 2m/(m+1)$. The velocity along these walls has the form $U = Kx^m$, which represents the freestream driving the boundary layer on the wall, with $x = 0$ at the tip of the wedge. The most prominent cases are:

$-2 \leq \beta \leq 0$, $-\frac{1}{2} \leq m \leq 0$: flow around an expansion corner of turning angle $\beta\pi/2$

$\beta = 0$, $m = 0$: the flat plate

$0 \leq \beta \leq +2$, $0 \leq m \leq \infty$: flow against a wedge of half-angle $\beta\pi/2$

$\beta = 1$, $m = 1$: the plane stagnation point (180° wedge)

$\beta = +4$, $m = -2$: doublet flow near a plane wall

$\beta = +5$, $m = -\frac{5}{3}$: doublet flow near a 90° corner

$\beta = +\infty$, $m = -1$: flow toward a point sink [i.e., the boundary-layer version of the Jeffery-Hamel flow in a convergent wedge (Sec. 3-8)].

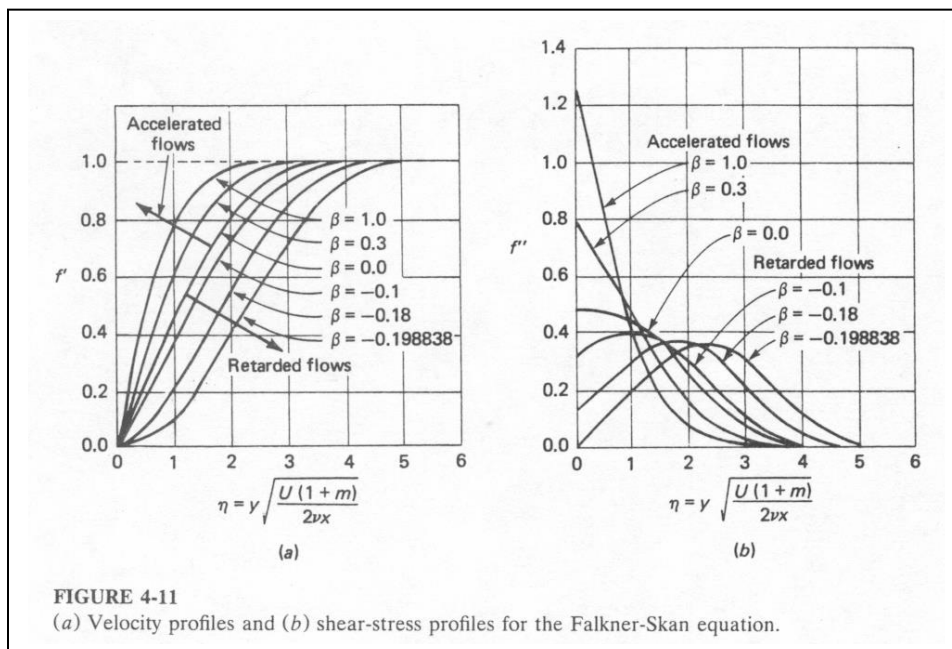
These are *similar* flows, i.e., for a given β , the velocity profiles all look alike when scaled by $U(x)$ and $\delta(x)$. They may also be used, with modest success, to predict the behavior of nonsimilar flows.

$0 \leq m \leq \infty$
 $0 \leq \beta \leq 2$
 Wedge Flow
 $m=0$
 $\beta=0$ } Flat Plate
 $m=1$
 $\beta=1$ } Stagnation Point

$m = -1$ $U = -1/x$
 $\beta = \infty$ $\gamma = \frac{y}{x} \sqrt{\frac{U}{\nu}}$
 Sink: Simple Sol
 involving tank of
 Sec. 4.37
 RL Sol
 of Jeffrey-Hamel
 flow

Expansion Corner
 $\beta = -1.98834$ (Separation)

Also, $\beta = 4, m = -2$: doublet flow near
 a plane wall
 $\beta = 5, m = -5/3$: doublet near a 90° corner



$u = U(x) f'$ where $U(x) = \frac{1}{2} x^m$
 ← velocity at edge of BL

$\beta = \frac{2m}{m+1}$ $\gamma = \frac{1}{2} \sqrt{g(x)} = \frac{1}{2} \left[\frac{m+1}{2} \frac{U(x)}{Ux} \right]^{1/2}$

$\delta(x) = \left[\frac{2\nu}{(m+1)\beta} \right] x^{(1-m)/2} = \frac{1}{2} \sqrt{\frac{\nu}{\beta x}} \left[\frac{m+1}{2} \frac{U(x)}{Ux} \right]^{1/2}$

$\delta^*(x) = \left(\frac{2}{m+1} \right)^{1/2} \left(\frac{\nu x}{U} \right)^{1/2} \int_0^{\infty} (1-f') dy$ $\left(\frac{2\nu}{(m+1)\beta} \right) x^{(1-m)/2}$

$\tau_w(x) = \mu \left(\frac{m+1}{2} \right)^{1/2} \left(\frac{\nu x}{U} \right)^{1/2} f''(0)$ $\mu \left(\frac{(m+1)\beta^2}{2\nu} \right) x^{(3m-1)/2}$

$\delta \propto x^{(1-m)/2}$ $\delta^* \propto x^{(1-m)/2}$ $\tau_w \propto x^{(3m-1)/2}$

Special Cases:

$U(x) = \text{const}$ 1. Blowing: $m=0$ $\delta \propto x^{1/2}$ $\delta^* \propto x^{1/2}$ $\tau_w \propto x^{-1/2}$

$U(x) = 2x$ 2. Stagnation Point: $m=1$ $\delta, \delta^* = \text{const}$ $\tau_w \propto x$

linearly increasing U during of BL exactly balanced by viscous diffusion such that $\delta, \delta^* = \text{const}$

$U = 2x^2$ 3. $m=3$: $\delta \propto x^{-1}$ $\delta^* \propto x^{-1}$ $\tau_w = \text{constant}$

acceleration rate from boundary increases τ_w exactly balanced by viscous diffusion spread momentum away from surface is reduce τ_w