ME:5160 (58:160) Intermediate Mechanics of Fluids Fall 2024 – HW3 Solution

P2.130 Consider a wooden cylinder (SG = 0.6) 1 m in diameter and 0.8 m long. Would this cylinder be stable if placed to float with its axis vertical in oil $(SG = 0.85)$?

Solution: A vertical force balance gives

$$
0.85 \pi R^{2} h = 0.6 \pi R^{2} (0.8 \text{ m}),
$$

or: $h = 0.565 \text{ m}$

$$
s = 0.6
$$

• M

$$
h = 0.8 \text{ m}
$$

$$
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$$

$$
h = 0.8 \text{ m}
$$

$$
s = 0.85
$$

The point B is at $h/2 = 0.282$ m above the bottom. Use Eq. (2.52) to predict the meta-center location:

MB =
$$
I_0/v_{sub}
$$
 = $[\pi(0.5)^4/4]/[\pi(0.5)^2(0.565)]$ = 0.111 m = MG + GB

Now GB = 0.4 m − 0.282 m = 0.118 m, hence **MG** = 0.111 − 0.118 = −**0.007 m**. This float position is thus **slightly unstable**. The cylinder would turn over. *Ans*. **P2.142** The tank of water in Fig. P2.142 is 12 cm wide into the paper. If the tank is accelerated to the right in rigid-body motion at 6 m/s2, compute (a) the water depth at AB, and (b) the water force on panel AB

Solution: From Eq. (2.55),

$$
\tan \theta = a_x/g = \frac{6.0}{9.81} = 0.612
$$
, or $\theta \approx 31.45^{\circ}$

Then surface point B on the left rises an additional $\Delta z = 12 \tan \theta \approx 7.34 \text{ cm}$,

or: water depth AB =
$$
9 + 7.34 \approx 16.3
$$
 cm Ans. (a)

The water pressure on AB varies linearly due to gravity only, thus the water force is

$$
F_{AB} = p_{CG} A_{AB} = (9790) \left(\frac{0.163}{2} \text{ m} \right) (0.163 \text{ m}) (0.12 \text{ m}) \approx 15.7 \text{ N} \quad Ans. \text{ (b)}
$$

P2.154 A very tall 10-cm-diameter vase contains 1178 cm³ of water. When spun steadily to achieve rigid-body rotation, a 4-cm-diameter dry spot appears at the bottom of the vase. What is the rotation rate, r/min, for this condition?

Solution: It is interesting that the answer has nothing to do with the water *density*. The value of 1178 cubic centimeters was chosen to make the rest depth a nice number:

$$
v = 1178
$$
cm³ = $\pi(5$ cm² H , solve $H = 15.0$ cm

One way would be to integrate and find the volume of the shaded liquid in Fig. P2.154 in terms of vase radius *R* and dry-spot radius r_o . That would yield the following formula:

$$
dv = \pi (R^2 - r_o^2) dz
$$
, but $z = \Omega^2 r^2 / 2g$, hence $dz = (\Omega^2 r / g) dr$
\nThus $v = \int_{r_o}^R \pi (R^2 - r_o^2) (\Omega^2 r / g) dr = \frac{\pi \Omega^2}{g} \int_{r_o}^R (R^2 r - r^3) dr = \frac{\pi \Omega^2}{g} (\frac{R^2 r^2}{2} - \frac{r^4}{4}) \Big|_{r_o}^R$
\nFinally: $v = \frac{\pi \Omega^2}{g} (\frac{R^4}{4} - \frac{R^2 r_o^2}{2} + \frac{r_o^4}{4}) = 0.001178 m^3$
\nSolve for $R = 0.05m$, $r_o = 0.02m$: $\Omega^2 = 3336$, $\Omega = 57.8 \frac{rad}{s} = 552 \frac{\text{r}}{\text{min}}$ Ans.

P3.115 A free liquid jet, as in Fig. P3.115, has constant ambient pressure and small losses; hence from Bernoulli's equation $z + V^2/(2g)$ is constant along the jet. For the fire nozzle in the figure, what are (a) the minimum and (b) the maximum values of θ for which the water jet will clear the corner of the building? For which case will the jet velocity be higher when it strikes the roof of the building?

Solution: The two extreme cases are when the jet just touches the corner A of the building. For these two cases, Bernoulli's equation requires that $V_1^2 + 2gz_1 = (100)^2 + 2g(0) = V_A^2 + 2gz_A = V_A^2 + 2(32.2)(50)$, or: $V_A = 82.3 \frac$ these two cases, Bernoulli's equation requires that
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\n
$$
V_1^2 + 2gz_1 = (100)^2 + 2g(0) = V_A^2 + 2gz_A = V_A^2 + 2(32.2)(50),
$$
 or: $V_A = 82.3 \frac{ft}{s}$

The jet moves like a frictionless particle as in elementary particle dynamics:

Vertical motion:
$$
z = (V_1 \sin \theta) t - \frac{1}{2}gt^2
$$
; Horizontal motion: $x = (V_1 \cos \theta) t$

Eliminate "t" between these two and apply the result to point A:

$$
z_{A} = 50 = x_{A} \tan \theta - \frac{gx_{A}^{2}}{2V_{1}^{2} \cos^{2} \theta} = 40 \tan \theta - \frac{(32.2)(40)^{2}}{2(100)^{2} \cos^{2} \theta};
$$
 clean up and rearrange:

$$
\tan \theta = 1.25 + 0.0644 \sec^{2} \theta, \text{ solve for } \theta = 85.94^{\circ} \text{ Ans. (a) and } 55.40^{\circ} \text{ Ans. (b)}
$$

Path (b) is shown in the figure, where the jet just grazes the corner A and goes over the top of the roof. Path (a) goes nearly straight up, to $z = 155$ ft, then falls down to pt. A. In both cases, the velocity when the jet strikes point A is the same, 82.3 ft/s.

P3.124 A necked-down section in a pipe flow, called a *venturi*, develops a low throat pressure which can aspirate fluid upward from a reservoir, as in Fig. P3.124. Using Bernoulli's equation with no losses, derive an expression for the velocity $V1$ which is just sufficient to bring reservoir fluid into the throat.

2; Bernoulli ($\Delta z = 0$): $p_1 + \frac{1}{2}\rho V_1^2 \approx p_{atm} + \frac{1}{2}\rho V_2^2$ 1 2 2 1 1 1 atm 2 1 1 Volume flow: V V (D /D) ; Bernoulli (z 0): p V p V = ρ gh. Hence:
 $\frac{1}{2} \rho V_1^2 \approx p_{\text{atm}} + \frac{1}{2}$ gin to aspirate into the throat when pa – p1 = ρ gh. Hence:
= $V_2 (D_2/D_1)^2$; Bernoulli ($\Delta z = 0$): $p_1 + \frac{1}{2} \rho V_1^2 \approx p_{atm} + \frac{1}{2} \rho V_2^2$

Solve for
$$
p_a - p_1 = \frac{\rho}{2} (\alpha^4 - 1) V_2^2 \ge \rho g h
$$
, $\alpha = \frac{D_2}{D_1}$, or: $V_2 \ge \sqrt{\frac{2gh}{\alpha^4 - 1}}$ Ans.

Similarly,
$$
V_{1,\text{min}} = \alpha^2 V_{2,\text{min}} = \sqrt{\frac{2gh}{1 - (D_1/D_2)^4}}
$$
 Ans.

C2.2 A prankster has added oil, of specific gravity SGo, to the left leg of the manometer at right. Nevertheless, the U-tube is still to be used to measure the pressure in the air tank. (a) Find an expression for *h* as a function of *H* and other parameters in the problem.

(b) Find the special case of your result when ptank = pa. (c) Suppose $H = 5$ cm, pa = 101.2 kPa, SGo = 0.85, and ptank is 1.82 kPa higher than pa. Calculate *h* in cm, ignoring surface tension and air density effects.

$$
p_i = p_a + \rho g H + \rho_w g (h - H) = p_{tank},
$$

 $p_i = p_a + \rho g H + \rho_w g (h - H) = p_{tank},$
 $\rho = SG_o \rho_w$ (ignore the column of air in the right leg)

Solve for:
$$
h = \frac{p_{tk} - p_a}{\rho_w g} + H(1 - SG_o)
$$
 Ans. (a)

If $ptank = pa$, then

$$
h = H(1 - SG_0) \quad \text{Ans. (b)}
$$

(c) For the particular numerical values given above, the answer to (a) becomes

$$
h = \frac{1820 \text{ Pa}}{998(9.81)} + 0.05(1 - 0.85) = 0.186 + 0.0075 = 0.193 \text{ m} = 19.3 \text{ cm} \quad \text{Ans. (c)}
$$

Note that this result is not affected by the actual value of atmospheric pressure.