

5.1 (also available as a Mathcad worksheet)

(a) $\hat{G} = \hat{H} - T\hat{S}$ at $P = 2.5 \text{ MPa}$ and $T = 223.99^\circ \text{C} = 497.14 \text{ K}$

$$\left. \begin{aligned} \hat{G}^{\text{V}} &= \hat{H}^{\text{V}} - T\hat{S}^{\text{V}} = 2803.1 - 497.14 \times 6.2575 = -307.8 \text{ J/g} \\ \hat{G}^{\text{L}} &= \hat{H}^{\text{L}} - T\hat{S}^{\text{L}} = 962.11 - 497.14 \times 2.5547 = -307.9 \text{ J/g} \end{aligned} \right\} \begin{array}{l} \text{equal with} \\ \text{the accuracy} \\ \text{of tables} \end{array}$$

(b)

$T(^{\circ}\text{C})$	$T(\text{K})$	$\hat{H}^{\text{V}}$	–	$T\hat{S}^{\text{V}}$	$\hat{G}^{\text{L}}$
225	498.15	2806.3	–	$498.15 \times 6.2639 =$	-314.1 J/g
250	523.15	2880.1	–	$523.15 \times 6.4085 =$	-472.5
300	573.15	3008.8	–	$573.15 \times 6.6438 =$	-799.1
350	623.15	3126.3	–	$623.15 \times 6.8403 =$	-1136.2
400	673.15	3239.3	–	$673.15 \times 7.0148 =$	-1482.7

(Note: All Gibbs free energies are relative to the internal energy and entropy of the liquid phase being zero at the triple point. Since $\hat{H}^{\text{L}} \sim \hat{U}^{\text{L}}$, and $\hat{G}^{\text{L}} = \hat{H}^{\text{L}} - T\hat{S}^{\text{L}}$, we have that $\hat{G}^{\text{L}} = 0$ at the triple point.)

(c)

$T(^{\circ}\text{C})$	$T(\text{K})$	$\hat{H}^{\text{L}}$	–	$T\hat{S}^{\text{L}}$	$\hat{G}^{\text{V}}$
160	433.15	675.55	–	$433.15 \times 1.9427 =$	-165.9 J/g
170	443.15	719.21	–	$443.15 \times 2.0419 =$	-185.7
180	453.15	763.22	–	$453.15 \times 2.1396 =$	-206.3
190	463.15	807.62	–	$463.15 \times 2.2359 =$	-227.9
200	473.15	852.45	–	$473.15 \times 2.3309 =$	-250.4
210	483.15	897.76	–	$483.15 \times 2.4248 =$	-273.8

RESULTS

(d)

$T(^{\circ}\text{C})$	150	160	180	200	220	224
$\hat{V}(\text{m}^3/\text{kg})$	0.001091	0.001102	0.001127	0.001157	0.001190	0.001197
						to
						0.07998

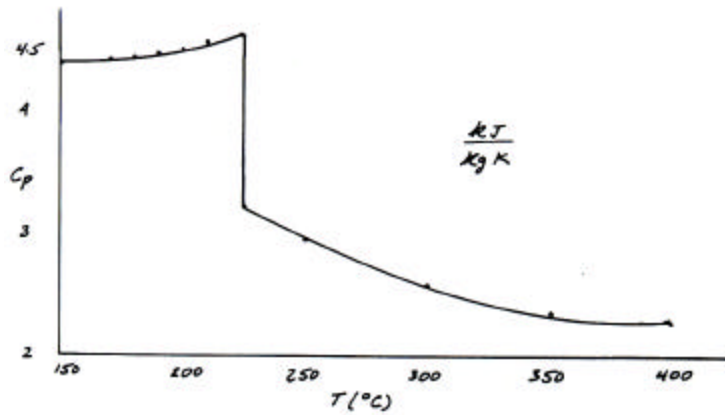
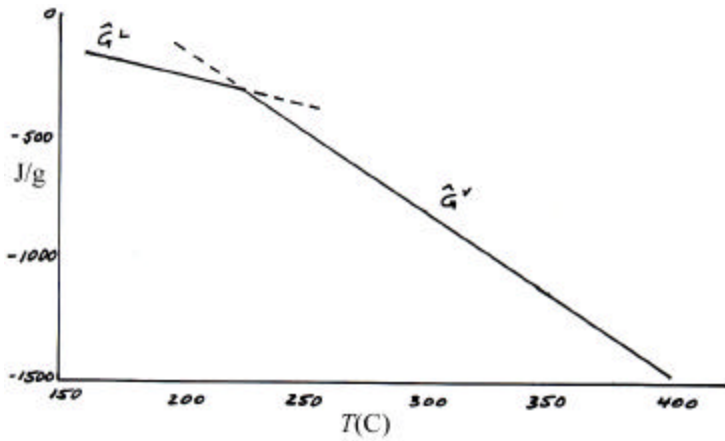
$T(^{\circ}\text{C})$	225	250	300	350	400
$\hat{V}(\text{m}^3/\text{kg})$	0.08027	0.08700	0.09890	0.10976	0.12010

(e) Will compute C_p from $C_p \sim \left(\frac{\Delta \hat{H}}{\Delta T} \right)_P = \frac{\hat{H}(T + \Delta T) - \hat{H}(T)}{\Delta T}$

$T(^{\circ}\text{C})$	150	170	180	190	200	210	224
							4.6225
$C_p(\text{kJ/kg K})$	4.328	4.392	4.430	4.472	4.518	4.572	to
							3.200

$T(^{\circ}\text{C})$	250	300	350	400
$C_p(\text{kJ/kg K})$	2.952	2.574	2.350	2.260

These results are plotted below.



5.2 Closed system energy balance: $\frac{dU}{dt} = \dot{Q} - P \frac{dV}{dt}$

Closed system entropy balance: $\frac{dS}{dt} = \frac{\dot{Q}}{T} + \dot{S}_{\text{gen}}$

(a) System at constant volume and constant entropy

$$\frac{dV}{dt} = 0 \quad \text{and} \quad \frac{dS}{dt} = 0$$

$$\Rightarrow \frac{dU}{dt} = \dot{Q} \quad \text{and} \quad 0 = \frac{\dot{Q}}{T} + \dot{S}_{\text{gen}} \Rightarrow \dot{Q} = -T\dot{S}_{\text{gen}}$$

$$\text{and } \frac{dU}{dt} = -T\dot{S}_{\text{gen}}; \quad T > 0; \quad \dot{S}_{\text{gen}} \geq 0$$

$$\Rightarrow \frac{dU}{dt} \leq 0 \quad \text{or } U = \text{minimum at equilibrium at constant } V \text{ and } S.$$

(b) System at constant entropy and pressure again $\dot{Q} = -T\dot{S}_{\text{gen}}$.

$$\text{Now } \frac{dP}{dt} = 0 \Rightarrow P \frac{dV}{dt} = \frac{d}{dt}(PV). \quad \text{Thus}$$

$$\frac{dU}{dt} = \dot{Q} - P \frac{dV}{dt} = -T\dot{S}_{\text{gen}} - \frac{d}{dt}(PV)$$

and

$$\frac{dU}{dt} + \frac{d}{dt}(PV) = \frac{d}{dt}(U + PV) = \frac{dH}{dt} = -T\dot{S}_{\text{gen}} \leq 0$$

Therefore, enthalpy is a minimum at equilibrium at constant S and P .