Chapter 3: Overview of Turbulent Flow Physics and Equations

Part 2: Reynolds-Averaged Navier-Stokes Equations

For convenience of notation use lower case with over squiggle, uppercase for mean, and lowercase for fluctuation in Reynolds decomposition.

$$\begin{array}{l} \sim \\ u_i = U_i + u_i \\ \sim \\ p = P + p \end{array}$$

$$\frac{\frac{\partial \widetilde{u}_i}{\partial x_i}}{\frac{\partial \widetilde{u}_i}{\partial t}} + \widetilde{u}_j \frac{\partial \widetilde{u}_i}{\partial x_i} = -\frac{1}{\rho} \frac{\partial \widetilde{p}}{\partial x_i} + \nu \frac{\partial^2 \widetilde{u}_i}{\partial x_j \partial x_j} - g \delta_{i3}$$

$$\longrightarrow \text{equation}$$

Mean Continuity Equation

$$\frac{\overline{\partial}}{\partial x_i} (U_i + u_i) = \frac{\partial U_i}{\partial x_i} + \frac{\partial \overline{u}_i}{\partial x_i} = \frac{\partial U_i}{\partial x_i} = 0$$

$$\frac{\partial u_i}{\partial x_i} = \frac{\partial U_i}{\partial x_i} + \frac{\partial u_i}{\partial x_i} = 0 \quad \rightarrow \quad \frac{\partial u_i}{\partial x_i} = 0$$

Both mean and fluctuation satisfy divergence = 0 condition.

Mean Momentum Equation

$$\frac{\partial}{\partial t}(U_i + u_i) + (U_j + u_j)\frac{\partial}{\partial x_j}(U_i + u_i)$$

$$= -\frac{1}{\rho}\frac{\partial}{\partial x_i}(P + p) + \nu \frac{\partial^2}{\partial x_j x_j}(U_i + u_i) - g\delta_{i3}$$

$$\frac{\overline{\partial}}{\partial t}(U_i + u_i) = \frac{\partial U_i}{\partial t} + \frac{\partial \overline{u}_i}{\partial t} = \frac{\partial U_i}{\partial t}$$

$$\overline{(U_j + u_j)} \frac{\partial}{\partial x_j} (U_i + u_i)$$

$$= U_j \frac{\partial U_i}{\partial x_j} + U_j \frac{\partial \overline{u}_i}{\partial x_j} + \overline{u_j} \frac{\partial V_i}{\partial x_j} + \overline{u_j} \frac{\partial u_i}{\partial x_j}$$

$$= U_j \frac{\partial U_i}{\partial x_i} + \frac{\partial}{\partial x_i} \overline{u_i u_j}$$

Since
$$\frac{\partial}{\partial x_j} \overline{u_i u_j} = \overline{u_j \frac{\partial u_j}{\partial x_j}} + \overline{u_j \frac{\partial u_i}{\partial x_j}} = \overline{u_j \frac{\partial u_i}{\partial x_j}}$$

$$\frac{\overline{\partial}}{\partial x_i}(P+p) = \frac{\partial P}{\partial x_i} + \frac{\partial \overline{p}}{\partial x_i} = \frac{\partial P}{\partial x_i}$$

$$-\overline{g\delta_{i3}} = -g\delta_{i3}$$

$$\overline{v} \frac{\partial^{2}}{\partial x_{j}^{2}} (U_{i} + u_{i}) = v \frac{\partial^{2} U_{i}}{\partial x_{j}^{2}} + v \frac{\partial^{2} \overline{u}_{i}}{\partial x_{j}^{2}} = v \frac{\partial^{2} U_{i}}{\partial x_{j}^{2}}$$

$$\frac{\partial U_{i}}{\partial t} + U_{j} \frac{\partial U_{i}}{\partial x_{j}} + \frac{\partial (\overline{u_{i}} \overline{u_{j}})}{\partial x_{j}} = -\frac{1}{\rho} \frac{\partial P}{\partial x_{i}} + v \frac{\partial^{2} U_{i}}{\partial x_{j}^{2}} - g \delta_{i3}$$
Or
$$\frac{\partial U_{i}}{\partial t} = -\frac{1}{\rho} \frac{\partial P}{\partial x_{i}} - g \delta_{i3} + \frac{\partial}{\partial x_{j}} \left[v \frac{\partial U_{i}}{\partial x_{j}} - \overline{u_{i}} \overline{u_{j}} \right]$$

$$\frac{\partial U_{i}}{\partial t} = -g \delta_{i3} + \frac{1}{\rho} \frac{\partial}{\partial x_{i}} \overline{\sigma}_{ij}$$

$$\overline{\sigma} = -P \delta_{ij} + \mu \left(\frac{\partial U_{i}}{\partial x_{j}} + \frac{\partial U_{j}}{\partial x_{i}} \right) - \rho \overline{u_{i}} \overline{u_{j}}$$
RANS
Equations
with
$$\frac{\partial U_{i}}{\partial x_{j}} = 0$$

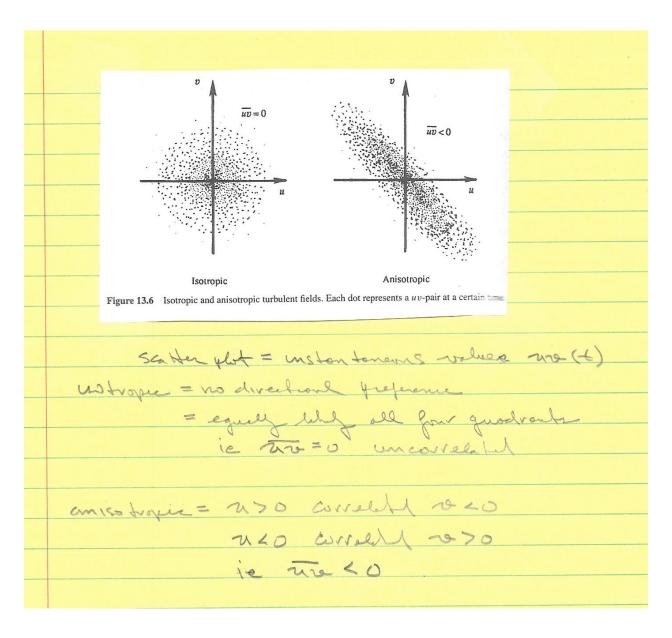
The difference between the NS and RANS equations is the Reynolds stresses $-\rho \overline{u_i u_j}$, which acts like additional stress.

$$-\rho \overline{u_i u_j} = -\rho \overline{u_j u_i} \quad \text{(i.e. Reynolds stresses are symmetric)}$$

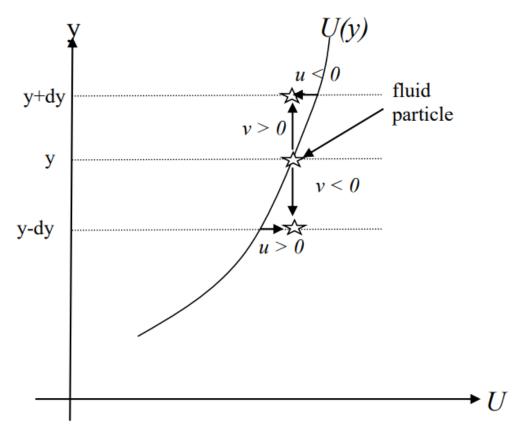
$$= \begin{bmatrix} -\rho \overline{u^2} & -\rho \overline{u} \overline{v} & -\rho \overline{u} \overline{w} \\ -\rho \overline{u} \overline{v} & -\rho \overline{v^2} & -\rho \overline{v} \overline{w} \\ -\rho \overline{u} \overline{v} & -\rho \overline{v} \overline{v} \end{bmatrix}$$

 $\overline{u_i^2}$ are normal stresses $\overline{u_i u_j}$ $i \neq j$ are shear stresses 6 new unknowns

For homogeneous/isotropic turbulence $\overline{u_i u_j}$ $i \neq j = 0$ and $\overline{u^2} = \overline{v^2} = \overline{w^2} = \text{constant}$; however, turbulence is generally non-isotropic.



Consider shear flow with $\frac{dU}{dy} > 0$ as below,



The fluid velocity is: $\underline{V} = (U + u, v, w)$

If fluid particle retains its total velocity \underline{V} from y to $y \pm dy$ gives, $U + u = constant \rightarrow \text{If } U$ increases, u decreases and vice versa.

$$\begin{array}{cccc}
v > 0 & \rightarrow & u < 0 \\
v < 0 & \rightarrow & u > 0
\end{array} \longrightarrow \begin{array}{c}
\overline{uv} < 0
\end{array}$$

x-momentum tends towards decreasing y as turbulence diffuses gradients and decreases $\frac{dU}{dv}$

x-momentum transport in y direction, i.e., across y = constant AA per unit area

$$M_{xy} = \int \rho \tilde{u} \underline{V} \cdot \underline{n} \, dA$$
, where $\tilde{u} = (U + u)$

$$\frac{d\overline{M_{xy}}}{dA} = \rho \overline{(U+u)v} = \rho U\overline{v} + \rho \overline{uv} = \rho \overline{uv}$$

i.e. $\rho \overline{u_i u_j}$ = average flux of j-momentum in i-direction = average flux of i-momentum in j-direction

Reynold verous Poisson equation
- = 02-P = Uijuiji P=P+P
= Dij Uji + Drini
con be obtained by John mean of 52P equation or 5. RANS equations

Anisotropy

Symmetry of the Reynolds stress tensor:

$$\overline{u_i u_j} = \overline{u_j u_i}$$

The diagonal components of the Reynolds stress tensor represent the normal stresses, which in general are not equal:

$$\overline{u_1^2}, \overline{u_2^2}, \overline{u_3^2}$$

The off-diagonal components represent the shear stresses:

$$\overline{u_i u_j}$$
 $i \neq j$

Turbulent kinetic energy per unit mass:

$$k(\underline{x},t) = \frac{1}{2}\underline{u} \cdot \underline{u} = \frac{1}{2}\overline{u_i u_i} = \frac{1}{2}\left(\overline{u_1^2} + \overline{u_2^2} + \overline{u_3^2}\right)$$

Anisotropy tensor:

$$a_{ij} = \overline{u_i u_j} - \frac{2}{3} k \delta_{ij}$$
Isotropic stress

Normalized anisotropy tensor:

$$b_{ij} = \frac{a_{ij}}{2k} = \frac{\overline{u_i u_j}}{\overline{u_i u_i}} - \frac{1}{3} \delta_{ij}$$

For isotropic turbulence $\overline{u_1^2} = \overline{u_2^2} = \overline{u_3^2}$ such that $k = \frac{3}{2} \overline{u_1^2}$

Role of the anisotropy tensor in the Mean Momentum Equation:

$$\rho \frac{D\overline{U_i}}{Dt} = -\rho g \delta_{i3} + \frac{\partial \overline{\sigma_{ij}}}{\partial x_j}$$

$$\overline{\sigma_{ij}} = -\overline{p} \delta_{ij} + \mu \left(\frac{\partial \overline{U_i}}{\partial x_j} + \frac{\partial \overline{U_j}}{\partial x_i} \right) - \rho \overline{u_i u_j}$$

$$\overline{u_i u_j} = \frac{2}{3} k \delta_{ij} + a_{ij} = 2k \left(\frac{1}{3} \delta_{ij} + b_{ij} \right)$$

$$\rho \frac{\partial \overline{u_i u_j}}{\partial x_j} + \frac{\partial \overline{p}}{\partial x_i} = \rho \frac{\partial a_{ij}}{\partial x_j} + \frac{\partial}{\partial x_i} \left(\overline{p} + \frac{2}{3} \rho k \right)$$

$$\overline{\sigma_{ij}} = -\overline{p} \delta_{ij} + \mu \left(\frac{\partial \overline{U_i}}{\partial x_j} + \frac{\partial \overline{U_j}}{\partial x_i} \right) - \rho \left(\frac{2}{3} k \delta_{ij} + a_{ij} \right)$$

$$\rho \frac{D\overline{U_i}}{Dt} = -\rho g \delta_{i3} - \frac{\partial}{\partial x_i} \left(\overline{p} + \frac{2}{3} \rho k \right) + \frac{\partial}{\partial x_j} \left[\mu \left(\frac{\partial \overline{U_i}}{\partial x_j} + \frac{\partial \overline{U_j}}{\partial x_i} \right) - \rho a_{ij} \right]$$

Therefore, only the anisotropic component a_{ij} is effective in transporting momentum since $\frac{2}{3}\rho k$ can be absorbed in a modified mean pressure.

Irrotational motion

Consider an irrotational random velocity field:

$$\underline{\widetilde{\omega}} = \underline{\Omega} + \underline{\omega} = 0$$

Both mean and fluctuating vorticity are equal to zero. For example, water waves and outer portion of turbulent jet (free shear flow) or boundary layer.

Notation: $u_{i,j} = \frac{\partial u_i}{\partial x_j}$, u_i = velocity fluctuation with $\underline{\omega} = 0$, i.e., $\omega_{ij} = \frac{1}{2} (u_{i,j} - u_{j,i}) = 0$ where ω_{ij} is the fluctuation rotation rate tensor.

$$u_{i,j} - u_{j,i} = 0$$

$$u_i (u_{i,j} - u_{j,i}) = 0 = \frac{u_i u_{i,j}}{u_{i,j}} - \frac{u_i u_{j,i}}{u_{i,j}}$$

$$\frac{\partial}{\partial x_i} (u_i u_j) = u_{i,i} u_j + u_i u_{j,i}$$

$$\frac{\partial}{\partial x_j} \left(\frac{1}{2} u_i u_i \right) = \frac{1}{2} \left(u_{i,j} u_i + u_i u_{i,j} \right) = u_i u_{i,j}$$

$$\frac{\partial}{\partial x_i} \left(\overline{u_i u_j} \right) = \frac{\partial}{\partial x_j} \left(\frac{1}{2} \overline{u_i u_i} \right) = \frac{\partial k}{\partial x_j} = \text{gradient of a scalar, i.e.,}$$

same form as fluctuating pressure: Corrsin-Kistler equation. Therefore, for potential flow, fluctuating velocity is equivalent to pressure fluctuations \rightarrow do not affect the mean velocity.

Closure Problem:

- 1. RANS equations differ from the NS equations due to the Reynolds stress terms
- 2. RANS equations are for the mean flow (U_i, P) ; thus, represent 4 equations with 10 unknowns due to the additional 6 unknown Reynolds stresses $\overline{u_i u_i}$
- 3. Equations can be derived for $\overline{u_i u_j}$ by summing products of velocity and momentum components and time averaging, but these include additionally 10 triple products $\overline{u_i u_j u_l}$ unknowns. Triple products represent Reynold stress transport.
- 4. Again, equations for triple products can be derived that involve higher order correlations leading to fact that RANS equations are inherently non-deterministic, which requires turbulence modeling.
- 5. Turbulence closure models render deterministic RANS solutions.
- 6. The NS and RANS equations have paradox that NS equations are deterministic but have nondeterministic solutions for turbulent flow due to inherent stochastic nature of turbulence, whereas the RANS equations are nondeterministic, but have deterministic solutions due to turbulence closure models.

	Closure Proken
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	Figure 1.8 A cylinder is towed through a quiescent fluid and $\mathbf{u}_{\mathbf{x}}$ is measured at location \mathbf{x}_{0} . The records of $\mathbf{u}_{\mathbf{x}}(t)$ in two nominally identical realizations of the experiment are quite different.
	2 (x, t) random
	Ti (X) and Ti ² (X) reproducible le Statistical proporties should be predictable
	so the con equations he derived for statistical
	poperties
	$e^{2} = -e^{2} \cdot \nabla^{2} - \nabla \rho + \mu \nabla^{2} u \qquad (1)$
	$u_{\ell} = F, (u, p)$
	A· \(\times = 0 \)
	D. (1) => D2(p/e) = -D.(21 D21)
	p(x) = 27 [7. (21.52)] dx' Cont
	ie u = F2 (u) for IC integrale in time "deforministical" find u(x,t) DNS !

However, impracticable for industrial use
at often Statistical variables of greatest
and often Statestical vorubles of greatest interest such as zi, zi etc. [zi(x, E) = zi(x) + zi(x, E)]
Weed equations to, to etc. However furns
out imposible to down equation for Statistical
variables or leady to hierarchy of Statistical
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higher order States trad warrabler
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 "Closure problem"
Arrow of Time
Arrow of Time
The arrow of time, also called time's arrow, is the concept positing the "one-way direction" or
"asymmetry" of time. It was developed in 1927 by the British astrophysicist virtual Eddington, could be
determined by studying the organization of atoms, molecules, and bodies, and might be drawn
upon a four-dimensional relativistic map of the world ("a solid block of paper").
Even equation 2 + 4 4.02 = -0(p/e)
in time revergedle, is, replace to My by
-t of -4 at con integrate Sachwards to
DS equations one not time reversestre!