## **Part 3: Momentum Integral Equation**

Historically similarity and other AFD methods used for idealized flows and momentum integral methods for practical applications, including pressure gradients, but failure 3D methods motivated 3D BL theory which quickly progressed to modern day CFD.

Momentum integral equation, which is valid for both laminar and turbulent flow:

$$\int_{y=0}^{\infty} (\text{steady flow BL equation} + (u - U) \text{ continuity}) \, dy$$

$$\frac{\tau_w}{\rho U^2} = \underbrace{\frac{1}{2}}_{C_f} = \frac{d\theta}{dx} + (2 + H) \frac{\theta}{U} \frac{dU}{dx}$$
For flat plate equation  $\Rightarrow \frac{dU}{dx} = 0$ 

$$\theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy$$

$$\delta^* = \int_0^{\delta} \left(1 - \frac{u}{U}\right) dy$$

$$H = \frac{\delta^*}{\theta}$$

Momentum:  $uu_x + vu_y = -\frac{\partial}{\partial x} \left(\frac{p}{\rho}\right) + \frac{1}{\rho} \frac{\partial \tau}{\partial y}$  where  $\tau = \mu \frac{\partial u}{\partial y}$ The pressure gradient evaluated form the outer potential flow using Bernoulli equation.

$$p + \frac{1}{2}\rho U^2 = \text{constant}$$
$$p_x + \frac{1}{2}\rho 2UU_x = 0$$
$$-p_x/\rho = UU_x$$

$$(u - U)\underbrace{\left(u_{x} + v_{y}\right)}_{Continuity} = uu_{x} + uv_{y} - Uu_{x} - Uv_{y}$$

$$\underbrace{uu_x + vu_y - UU_x - \frac{1}{\rho}\tau_y}_{0} + \underbrace{uu_x + uv_y - Uu_x - Uv_y}_{0} = 0$$

$$-\frac{1}{\rho}\tau_{y} = -2uu_{x} - vu_{y} + UU_{x} - uv_{y} + Uu_{x} + Uv_{y}$$
$$= \frac{\partial}{\partial x}(uU - u^{2}) + (U - u)U_{x} + \frac{\partial}{\partial y}(vU - vu)$$

$$\int_{0}^{\infty} -\frac{1}{\rho} \tau_{y} dy = -(\tau_{\infty}^{\prime} - \tau_{w})/\rho = \frac{\partial}{\partial x} \int_{0}^{\infty} u(U-u) dy + U_{x} \int_{0}^{\infty} (U-u) dy + (vU - vu) \Big|_{0}^{\infty}$$

$$\frac{\tau_w}{\rho} = \frac{\partial}{\partial x} \left[ U^2 \int_0^\infty \frac{u}{U} \left( 1 - \frac{u}{U} \right) dy \right] + U_x U \int_0^\infty \left( 1 - \frac{u}{U} \right) dy$$
$$= U^2 \theta_x + 2U U_x \theta + U U_x \delta^*$$

$$\frac{\tau_w}{\rho U^2} = \frac{1}{2}C_f = \theta_x + (2\theta + \delta^*)\frac{1}{U}\frac{dU}{dx}$$
$$\frac{C_f}{2} = \frac{d\theta}{dx} + (2 + H)\frac{\theta}{U}U_x$$

TABLE 41 Boundary-layer predictions from five piecewise analytic profiles with their errors relative to the classic Blasius values  $\frac{u}{U} = F(\xi)$  $\eta^0 = \frac{\delta^0}{\delta}$  $\theta^{*} = \frac{\theta}{s}$  $H = \frac{\delta^*}{\theta}$  $C_f \sqrt{Re_s} = \frac{\delta^2}{x} \sqrt{Re_s}$  $\frac{\delta}{r} \sqrt{Re_s}$ L<sub>2</sub> error L2=[[(F-Fa)] dy  $2\xi - \xi^2$ 0.333 0.133 2.500 1 5.477 0.730 1.826 0.020 3.1% 0.25% 3.5% 9.5% 10% 6.1% 32-300 0.375 0.139 2 2.692 4.641 0.646 1.740 0.034 9.0% 4.7% 4.0% 7.2% 2.6% 1.1% 3  $2\xi - 2\xi^3 + \xi^4$ 0.300 0.118 2.554 5.836 0.685 1.751 0.054 13% 12% 1.4% 3.2% 17% 1.8% ÷  $\sin(\frac{1}{2}\pi_i^2)$ 0.363 0.137 2.660 0.655 4,795 1.743 0.021 5.6% 2.7% 2.7% 4.1% 1.3% 1.3% 5 32-83+38 0.350 0.134 2.618 4.993 0.668 1.748 0.008 1.7% 0.52% 1.1% 0.13% 0.53% 1.6% Blasius (1908) 0.344 0.133 2.59 5 0.664 1.72 n/aPoll housen (1921) 1,2,3 4 Sohlichly (1979) S Majdeloui 1 Xuon (2020) Pohlhousen paradax " mucacy only , ic, # & yroph can sature does not improve BC: M(X, 0)=0 1 10 slip 21(x,5)= 5 1 = mater Ny (4,5)=0 = Smisoth marge 3 MAYy (x,0) = Px & correct Sulence momentum y=0 nyy (y, 5)= 0 = May Ty = 0 yers shear shim at 5 However, the Blesnes fifthe does not in fast saturly all there conditions ! When I Saberfin 1-3 of 2-5 Saberfung 1-4 but only 3 Saberfun 1-5 Classet Le enor

$$\begin{split} & \mathcal{S}_{2} \leq \mathcal{S}_{2} < \mathcal{S}_{2} \leq \mathcal{S}_{2} < \mathcal{S}_$$

## **Thwaites Method (1949)**

Pressure gradient parameter  $\lambda = \frac{\theta^2}{\nu} \frac{dU}{dx} = (\frac{\theta}{\delta})^2 \Lambda$  where  $\Lambda = \frac{\delta^2}{\nu} \frac{dU}{dx} = -p_x \frac{\delta^2}{\mu U}$  is the Pohlhausen parameter.

Multiply momentum integral equation by  $\frac{U\theta}{v}$ 

$$\frac{\tau_w\theta}{\mu U} = \frac{U\theta}{v}\frac{d\theta}{dx} + \frac{\theta^2}{v}\frac{dU}{dx}(2+H)$$

The equation is dimensionless and, LHS and H can be correlated with  $\lambda$  as shear and shape-factor correlations:

$$\frac{\tau_w \theta}{\mu U} = S(\lambda) = (\lambda + 0.09)^{0.62}$$
$$H = \delta^* / \theta = H(\lambda) = \sum_{i=0}^5 a_i (0.25 - \lambda)^i$$

$$a_i = (2, 4.14, -83.5, 854, -3337, 4576)$$

Note

$$\frac{U\theta}{v}\frac{d\theta}{dx} = \frac{1}{2}U\frac{d}{dx}\left(\frac{\theta^2}{v}\right)$$

Substitute above into momentum integral equation.

$$S(\lambda) = \frac{1}{2}U\frac{d}{dx}\left(\frac{\theta^2}{\nu}\right) + \lambda(2+H)$$
$$U\frac{d(\lambda/U_x)}{dx} = 2[S - \lambda(2+H)\lambda] = F(\lambda)$$

 $F(\lambda) = 0.45 - 6\lambda$  based on AFD and EFD

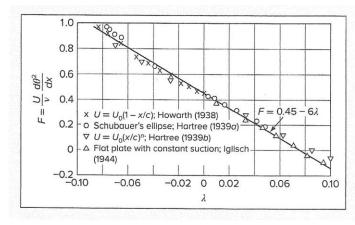


FIGURE 4-27 Empirical correlation of the boundary-layer function in Eq. (4-156). [*After Thwaites (1949)*.]

Define 
$$z = \frac{\theta^2}{\nu}$$
 so that  $\lambda = z \frac{dU}{dx}$ 

$$U\frac{dz}{dx} = 0.45 - 6\lambda = 0.45 - 6z\frac{dU}{dx}$$

$$U\frac{dz}{dx} + 6z\frac{dU}{dx} = 0.45$$

$$\frac{1}{U^5}\frac{d}{dx}(zU^6) = U\frac{dz}{dx} + 6z\frac{dU}{dx} = 0.45$$

$$d(zU^6) = 0.45U^5 dx$$

$$zU^6 = 0.45 \int_0^x U^5 dx + C$$

$$\Rightarrow \theta^2 = \theta_0^2 + \frac{0.45\nu}{U^6} \int_0^x U^5 dx$$

 $\theta_0(x = 0) = 0$  and U(x) known from potential flow solution.

Complete solution:

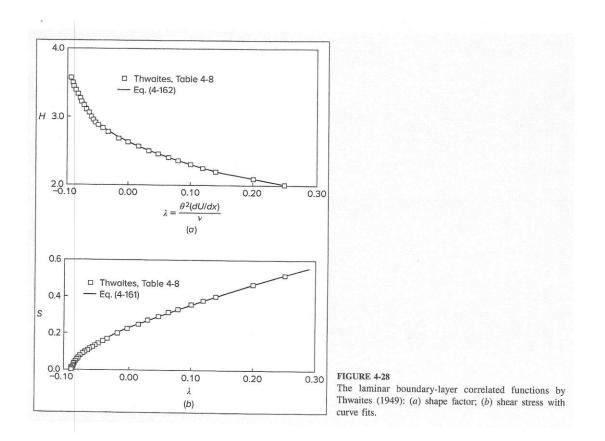
$$\lambda = \lambda(\theta) = \frac{\theta^2}{\nu} \frac{dU}{dx}$$
$$\frac{\tau_w \theta}{\mu U} = S(\lambda)$$
$$\delta^* = \theta H(\lambda)$$

Accuracy: mild  $p_x$   $\pm\,5\%$  and strong adverse  $p_x$   $(\tau_w~near~0)~\pm\,15\%$ 

## TABLE 4-8

# Shear and shape functions correlated by Thwaites (1949)

λ	$H(\lambda)$	$S(\lambda)$	λ	$H(\lambda)$	S(l)
+0.25	2.00	0.500	-0.056	2.94	0.122
0.20	2.07	0.463	-0.060	2.99	0.113
0.14	2.18	0.404	-0.064	3.04	0.104
0.12	2.23	0.382	-0.068	3.09	0.095
0.10	2.28	0.359	-0.072	3.15	0.085
+0.080	2.34	0.333	-0.076	3.22	0.072
0.064	2.39	0.313	-0.080	3.30	0.056
0.048	2.44	0.291	-0.084	3.39	0.038
0.032	2.49	0.268	-0.086	3.44	0.027
0.016	2.55	0.244	-0.088	3.49	0.015
0.0	2.61	0.220	-0.090	3.55	0.000
				(Separation)	
-0.016	2.67	0.195			
-0.032	2.75	0.168			
-0.040	2.81	0.153			
-0.048	2.87	0.138			
-0.052	2.90	0.130			



Separation predicted within 4%; however, large scale separation causes viscous/inviscid interaction and alters imposed external U(x) and  $p_x(x)$ 

#### TABLE 4-9

Laminar-separation-point prediction by Thwaites' method

		Thwaites		
U(x)	$x_{sep}$ (exact)	x <sub>sep</sub>	Error [%]	
Howarth (1938)				
1 - x	0.120	0.123	+2.5	
Tani (1949)		0.00	72.5	
$1 - x^2$	0.271	0.268	-1.1	
$1 - x^4$	0.462	0.449	-2.8	
$1 - x^8$	0.640	0.621	-3.0	
Terrill (1960)			5.0	
sin(x)	1.823	1.800	-1.3	
Curle (1958)			1.5	
$x - x^3$	0.655	0.648	-1.1	
Görtler (1957)				
$\cos(x)$	0.389	0.384	-1.3	
$(1-x)^{1/2}$	0.218	0.221	+1.3	
$(1 - x)^2$	0.0637	0.0652	+2.4	
$(1 + x)^{-1}$	0.151	0.158	+4.6	
$(1 + x)^{-2}$	0.0713	0.0739	+3.6	

### **Pohlhausen Velocity Profile:**

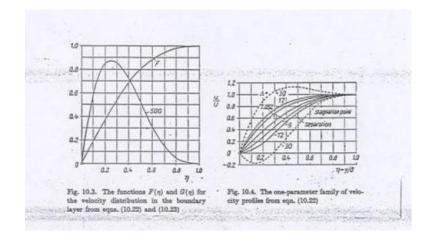
$$\frac{u}{u} = f(\eta) = a\eta + b\eta^{2} + c\eta^{3} + d\eta^{4} \text{ with } \eta = \frac{y}{\delta}$$
a, b, c, d determined from boundary conditions:  
1)  $y = 0 \rightarrow u = 0, u_{yy} = -\frac{U}{v}U_{x}$   
2)  $y = \delta \rightarrow u = U, u_{y} = 0, u_{yy} = 0$   
 $\Rightarrow \frac{u}{U} = F(\eta) + \Lambda G(\eta), -12 \leq \Lambda \leq 12 \quad \Lambda = \frac{\delta^{2}}{v}\frac{dU}{dx} = -p_{x}\frac{\delta^{2}}{\mu U}$   
separation (experiment:  $\Lambda_{separation} = -5$ )

$$F(\eta) = 2\eta - 2\eta^{3} + \eta^{4}$$
  

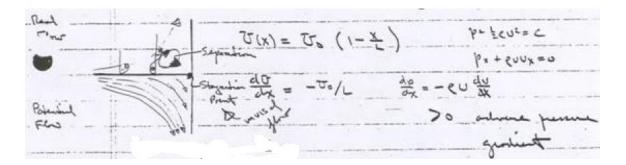
$$G(\eta) = \frac{\eta}{6} (1 - \eta)^{3}$$
  

$$\lambda = \lambda(\Lambda) = \left(\frac{37}{315} - \frac{\Lambda}{945} + \frac{\Lambda^{2}}{9072}\right)\Lambda$$

Profiles are realistic, except near separation. In guessed profile methods u/U directly used to solve momentum integral equation numerically, but accuracy not as good as empirical correlation methods; therefore, use Thwaites method to get  $\lambda$ , etc., and then use  $\lambda$  to get  $\Lambda$  and plot u/U.



Howarth linearly decelerating flow (example of exact solution of steady state 2D boundary layer)



Howarth proposed a linearly decelerating external velocity distribution  $U(x) = U_0 \left(1 - \frac{x}{L}\right)$  as a theoretical model for laminar boundary layer study. Use Thwaites's method to compute:

a)  $X_{sep}$ b)  $C_f\left(\frac{x}{L}=0.1\right)$ 

Note  $U_x = -U_0/L$ 

Solution

$$\theta^{2} = \frac{0.45\nu}{U_{0}^{6}\left(1 - \frac{x}{L}\right)^{6}} \int_{0}^{x} U_{0}^{5}\left(1 - \frac{x}{L}\right)^{5} dx = 0.075 \frac{\nu L}{U_{0}} \left[ \left(1 - \frac{x}{L}\right)^{-6} - 1 \right]$$

can be evaluated for given L, Re<sub>L</sub>

$$\lambda = \frac{\theta^2}{\nu} \frac{dU}{dx} = -0.075 \left[ \left( 1 - \frac{x}{L} \right)^{-6} - 1 \right]$$
$$\lambda_{sep} = -0.09 \Rightarrow \frac{X_{sep}}{L} = 0.123$$

3% higher than exact solution =0.1199

$$C_f \left(\frac{x}{L} = 0.1\right) \rightarrow \text{i.e. just before separation}$$
$$\lambda = -0.0661$$
$$S(\lambda) = 0.099 = \frac{1}{2}C_f Re_{\theta}$$
$$C_f = \frac{2(0.099)}{Re_{\theta}}$$

Compute  $Re_{\theta}$  in terms if  $Re_L$ 

$$\theta^{2} = 0.075 \frac{\nu L}{U_{0}} [(1 - 0.1)^{-6} - 1] = 0.0661 \frac{9L}{U_{0}}$$

$$\frac{\theta^{2}}{L^{2}} = 0.0661 \frac{\nu L}{U_{0}} = \frac{0.0661}{\text{Re}_{L}}$$

$$\frac{\theta}{L} = \frac{0.257}{\text{Re}_{L}^{\frac{1}{2}}}$$

$$\text{Re}_{\theta} = \frac{\theta}{L} \text{Re}_{L} = 0.257 \text{Re}_{L}^{\frac{1}{2}}$$

$$C_{f} = \frac{2(0.099)}{0.257} \text{Re}_{L}^{-\frac{1}{2}} = 0.77 \text{Re}_{L}^{-\frac{1}{2}}$$
To complete solution must specify Re<sub>L</sub>

Consider the complex potential  

$$F(z) = \frac{a}{2}z^{2} = \frac{a}{2}r^{2}e^{2i\theta}$$

$$\varphi = \operatorname{Re}[F(z)] = \frac{a}{2}r^{2}\cos 2\theta$$

$$\psi = \operatorname{Im}[F(z)] = \frac{a}{2}r^{2}\sin 2\theta$$
Orthogonal rectangular hyperbolas
$$\varphi: \operatorname{asymptotes} y = \pm x$$

$$\psi: \operatorname{asymptotes} y = \pm x$$

$$\psi: \operatorname{asymptotes} y = 0$$

$$\left\{ \underbrace{V} = \nabla \varphi = \varphi_{r}\hat{e}_{r} + \frac{1}{r}\varphi_{\rho}\hat{e}_{\theta} \qquad \underbrace{\hat{e}_{r} = (\cos 2 + \sin \theta)}_{\hat{e}_{r} = -i\pi \epsilon 1 + \sin \theta} \right\}$$

$$v_{r} = ar \cos 2\theta$$

$$v_{r} = ar \cos 2\theta$$

$$V_{r} = ar \cos 2\theta$$

$$V_{r} = \cos \theta + \sin \theta\hat{f} + (v_{r} \sin \theta + v_{\theta} \cos \theta)\hat{f}$$
Potential flow slips along surface: (consider  $\theta = 90^{\circ}$ )
$$1) \text{ determine } a \text{ such that } v_{r} = U_{0} \text{ at } r = L, \theta = 90^{\circ}$$

$$v_{r} = aL \cos(2 \times 90) = U_{0} \Rightarrow aL = -U_{0}, \text{ i.e. } a = -\frac{U_{0}}{L}$$

$$\varphi = (v_{1}(x) = -a(L - x)) = \frac{U_{0}}{L}(L - x) = U_{0}(1 - \frac{x}{L})$$

$$(v_{x} = -\frac{U_{0}}{L}$$

$$\varphi = -\frac{U_{0}}{L} \quad (v_{x} = -\frac{U_{0}}{L})$$

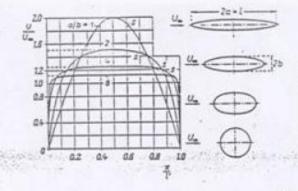


Fig. 10.9. Potential velocity distribution function on elliptical cylinders of alcoderness  $a_jb = 1, 2, 4, 8$ , the direction of the stream being parallel to the major axis

S - position of point of separation

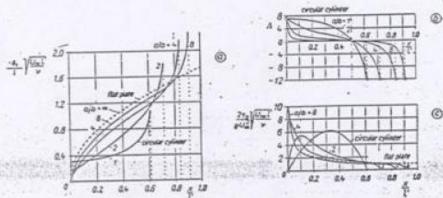


Fig. 10.10. Results of the calculation of boundary layers on elliptical cylinders of alenderness a/b = 1, 2, 4, 8. Fig. 10.9. a) displacement thickness of the boundary layer, b) shape factor c) shearing stress at the wall, 2  $t' = \operatorname{circumference}$  of the ellipse; a/b = 1 circular cylinder;  $a/b = \infty$  flat plate

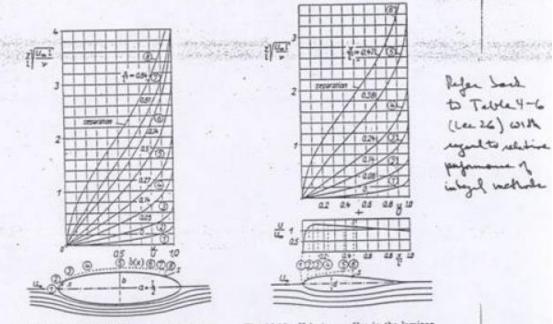


Fig. 10.11. Velocity profiles in the laminar boundary layer on an elliptical cylinder. Ratio of axes  $a/\delta = 4$ 

Fig. 10.12. Velocity profiles in the laminar boundary layer and potential velocity function for a Zhukovskii serofoil J 015 of thickness ratio d/l = 0.15 at an angle of incidence  $\alpha = 0$ 

Reduce devertion momentum integrit equation 
$$\frac{1}{2}$$
  

$$\frac{\pi (y_{1})_{x}}{\pi (y_{0})_{x}} = \frac{1}{2} \frac{1$$

$$S \qquad S$$

$$\frac{1}{2\pi} \int u(\overline{v} - v) A_{y} + \overline{v} + \overline{v} \int (\overline{v} - v) A_{y} = \overline{v} - \sqrt{2}$$

$$\frac{1}{2\pi} \int u(\overline{v} - v) A_{y} + \overline{v} + \overline{v} + \overline{v} \int ((1 - \frac{v}{2}) A_{y} = \frac{v}{2} - \sqrt{2}$$

$$\frac{1}{2\pi} \int \frac{1}{2\pi} \int \frac{1}{2\pi$$

Known - Poil basen would  
"1/15 = 
$$n + b \eta + c \eta^{2} + \lambda \eta^{3} + c \eta^{4} - \eta(x_{1}\eta) = \frac{u}{2}/5(x)$$
  
where  $n-c = \frac{1}{2}(x)$  is not annoted intervalue  
 $n(x_{1}\eta) = 0$   $n(x_{1}\eta) = -\overline{U(x)}$   $\overline{U_{x}}$   $n_{2\eta}(x_{1}\eta) = 0$   
 $u_{y}(x_{1}\eta) = 0$   $n(x_{1}\eta) = -\overline{U(x)}$   $\overline{U_{x}}$   $n_{2\eta}(x_{1}\eta) = 0$   
 $u_{y}(x_{1}\eta) = 0$   $n(x_{1}\eta) = -\overline{U(x)}$   $\overline{U_{x}}$   $n_{2\eta}(x_{1}\eta) = 0$   
 $u_{y}(x_{1}\eta) = 0$   $n(x_{1}\eta) = -\overline{U(x)}$   $\overline{U_{x}}$   $n_{2\eta}(x_{1}\eta) = 0$   
 $u_{y}(x_{1}\eta) = 0$   $n(x_{1}\eta) = -\frac{1}{2}t$   $\overline{U_{x}} = -\lambda(x)$   
 $\overline{U_{x}}$   $\overline{U_{y}} = \frac{1}{2}t$   $\overline{U_{x}} = -\lambda(x)$   $\overline{J=0}$   
 $n_{y}(x_{1}) = 0$   $n(x_{1}) = n_{\eta} \frac{1}{2} = 0$   $\overline{J=1}$   
 $\overline{U_{x}} = \frac{1}{2}t$   $\overline{U_{x}} = \frac{1}{2}t (\overline{U_{x}}) = \frac{1}{2}t \frac{1}{2}t - \frac{1}{2}t$   
 $\overline{U_{x}} = \frac{1}{2}t \frac{1}{2}t (\overline{U_{x}}) = n_{\eta} \frac{1}{2}t - \frac{1}{2}t \frac{1}$ 

$$\frac{2}{200} = (2+\frac{2}{2}) \frac{2}{20} \frac{1}{2} \frac{1$$

Schoon procedure:  
1. 
$$Tr(x)$$
  
2.  $P(x)$   
3.  $J_{n}(x)$  from  $(\frac{21}{21} - \frac{3}{24} - \frac{3}{24}) \int_{-\infty}^{\infty} = \frac{O^{2}}{7} U_{x}$  with  
 $\frac{1}{2} \int_{-\infty}^{\infty} \frac{1}{24} \int_$ 

til equation # 2 mille BL when i a me ~ 148, mgg, etc. =0 Astanx + renz = ucnex + A nyy 0 1= # 24 = - To/e [ unx - nevex + very 12= 28 ly uxy = vuzdy= ny WAZ= WZwzuxly W=-NXY + mixely - de= wydy t= 2 W21 - SEND mux - nenex - neux + mux] dy = - To/e [" (nex - 2/x + m - -unex - { ( (ne-n) ver dy = - To/e ) + (ac - 21 ) 24 (1- 1/2) dy = To/e sne The ing] + nevex 54 Ax [n (ne- 2)] = nx (ne-2) + n (nex - 11x) A (2229) + never 5 = To/e

$$\frac{1}{2} \frac{1}{2} \frac{1}$$

Alfinetic Animation momentum why for equation the s  
North Mark to run = 21624 + 
$$\frac{1}{6}$$
 Tay  
 $21624 + 25 Ty$   
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 $21624 + 20 Ty = 2001 + 2001 - 200 Here +  $\frac{1}{6}$  Ty  
 $21624 + 2001 - 200 Here = -701/2$   
 $0 - -2001$   
 $\int [(14)_{x} - 16244_{x}] A_{y} + 4000 - -701/2 - 2000$   
 $\int [(14)_{x} - 16244_{x}] A_{y} + 4000 - -701/2$   
 $0 - 200 - 2000 - 2$$ 

Example Momentum integal Ja(x) = (Jo/L)x menty flow is Stognation part flow FIL with M=I S(x) = Jvx/02 = [v1/00]12 = crusting U=1x = 5x constant ~ 1ve= f!(y) 7=8/8 8"= 5 × constant Lade 0 1 5+ integrale velocity 7= [.vx Je(x)]12- f(y) profile so do  $u = Y_{2} = \left[ U \times \frac{U_{0}}{2} \times \int^{V_{2}} f'(\gamma) \right]$ Zw/e = Ax [ 10 x2 0] + Tox 5 (Ax [ Unx] [VL/00]1/2 = vox f'(7) = 2002 × 0 + 002 × 51 L2 = Jef'(7)  $\frac{Zw}{2ev_{2}^{2}} = \left(\frac{40+25x}{L}\right)\frac{x}{L} = ax \quad i \in masses$ linearly one equation three unknown: "Tw, O, 5" Con une sharifer method to solve (or Karmon - Pohl heusen)

#### EXAMPLE 10.6

Use Thwaites' method to estimate the momentum thickness, displacement thickness, and see shear stress of the Blasius boundary layer with  $\theta_0 = 0$  at x = 0.

#### Solution

The solution plan is to use (10.50) to obtain  $\theta$ . Then, because  $dU_e/dx = 0$  for the Blasius boundarylayer,  $\lambda = 0$  at all downstream locations and the remaining boundary-layer parameters can determined from the  $\theta$  results, (10.45), (10.46), and Table 10.2. The first step is setting  $U_e = U =$ constant in (10.50) with  $\theta_0 = 0$ :

$$\theta^2 = \frac{0.45\nu}{U^6} \int_0^{\hat{U}} U^5 dx = \frac{0.45\nu}{U} x, \text{ or } \theta = 0.671 \sqrt{\frac{\nu x}{U}}$$

This approximate answer is 1% higher than the Blasius-solution value. For  $\lambda = 0$ , the tabulate shape factor is H(0) = 2.61, so:

$$\delta^* = \theta\left(\frac{\delta^*}{\theta}\right) = \theta H(0) = 0.671 \sqrt{\frac{\nu x}{U}}(2.61) = 1.75 \sqrt{\frac{\nu x}{U}}$$

This approximate answer is also 1% higher than the Blasius-solution value. For  $\lambda = 0$ , the shear correlation value is l(0) = 0.220, so:

$$\tau_w = \mu \frac{U}{\theta} l(0) = \frac{\mu U}{0.671\sqrt{\nu x/U}} (0.220) = \frac{1}{2} \rho U^2(0.656) \sqrt{\frac{\nu}{Ux}},$$

which implies a skin friction coefficient of:

$$C_f = \frac{\tau_w}{\frac{1}{2}\rho U^2} = \frac{0.656}{\sqrt{\mathrm{Re}_x}},$$

which is 1.2% below the Blasius-solution value.

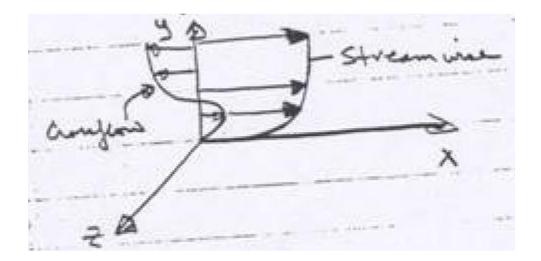
K= - UX

N=K

Lorrelations.

## **3-D Integral methods**

Momentum integral methods perform well (i.e. compare well with experimental data) for a large class of both laminar and turbulent 2D flows. However, for *3D flows they do not*, primarily due to the inability of correlating the crossflow velocity components.



The cross flow is driven by  $\frac{\partial p}{\partial z}$ , which is imposed on BL from the outer potential flow U(x,z).

3-D boundary layer equations

$$u_{x} + v_{y} + w_{z} = 0;$$
  

$$uu_{x} + vu_{y} + wu_{z} = -\frac{\partial}{\partial x}(p/\rho) + vu_{yy} - \frac{\partial}{\partial y}(\overline{u'v'})$$
  

$$uw_{x} + vw_{y} + ww_{z} = -\frac{\partial}{\partial z}(p/\rho) + vw_{yy} - \frac{\partial}{\partial y}(\overline{v'w'})$$
  
+ closure equations

Differential methods have been developed for this reason as well as for extensions to more complex and non-thin boundary layer flows.