## The exam is closed book and closed notes.

A thin flat plate 20 by 40 cm is immersed in a $1-\mathrm{m} / \mathrm{s}$ stream of water at $20^{\circ} \mathrm{C}(\rho=998 \mathrm{~kg} / \mathrm{m} 3, \mu$ $=0.001 \mathrm{~kg} / \mathrm{m} . \mathrm{s}$.). Assume that the flow is laminar for $R e_{x}<5 \mathrm{E} 5$ and turbulent for larger $R e_{x}$. (a) If the stream is parallel to the short side of the plate, compute the boundary layer thickness at the end of the plate (in stream-wise direction), and the water velocity at a point 1 mm normal to the end of the plate. (b) If the stream is parallel to the long side, compute the wall shear stress at the end of the plate (in stream-wise direction), and the total friction drag considering both front and back sides of the plate.

## Equations:

- The Blasius solution for laminar boundary layer flow shows that the dimensionless velocity profile $u / U$ is a function only of the single composite dimensionless variable $\eta=y\left(\frac{U}{v x}\right)^{1 / 2}$. Accurate solution for the function is obtained only by numerical integration and some tabulated values of the velocity profile shape are given in the Table below:

| $y[U /(\nu x)]^{1 / 2}$ | $u / \boldsymbol{U}$ | $y[U /(\nu x)]^{1 / 2}$ | $u / U$ |
| :---: | :---: | :---: | :---: |
| 0.0 | 0.0 | 2.8 | 0.81152 |
| 0.2 | 0.06641 | 3.0 | 0.84605 |
| 0.4 | 0.13277 | 3.2 | 0.87609 |
| 0.6 | 0.19894 | 3.4 | 0.90177 |
| 0.8 | 0.26471 | 3.6 | 0.92333 |
| 1.0 | 0.32979 | 3.8 | 0.94112 |
| 1.2 | 0.39378 | 4.0 | 0.95552 |
| 1.4 | 0.45627 | 4.2 | 0.96696 |
| 1.6 | 0.51676 | 4.4 | 0.97587 |
| 1.8 | 0.57477 | 4.6 | 0.98269 |
| 2.0 | 0.62977 | 4.8 | 0.98779 |
| 2.2 | 0.68132 | 5.0 | 0.99155 |
| 2.4 | 0.72899 | $\infty$ | 1.00000 |
| 2.6 | 0.77246 |  |  |

And the laminar boundary layer thickness is computed as: $\frac{\delta}{x} \sim \frac{5.0}{R e_{x}^{1 / 2}}$ where $R e_{x}=\frac{U x}{v}$

- Laminar Boundary Layer: $c_{f}=\frac{2 \tau_{w}}{\rho U^{2}}=\frac{0.664}{R e_{x}^{1 / 2}} ; C_{D}=\frac{D}{0.5 \rho A U^{2}}=\frac{1.328}{R e_{L}^{1 / 2}}$;
- Turbulent Boundary Layer: $c_{f}=\frac{2 \tau_{w}}{\rho U^{2}} \approx \frac{0.027}{R e_{x}^{1 / 7}} ; C_{D}=\frac{D}{\frac{1}{2} \rho A U^{2}}=\frac{0.031}{R e_{L}^{1 / 7}}$; velocity profile: $\frac{u}{U} \approx\left(\frac{y}{\delta}\right)^{\frac{1}{7}}$ where $\frac{\delta}{x} \approx \frac{0.16}{R e_{x}^{1 / 7}}$


## Solution:

(a)

$$
\begin{gather*}
R e_{x=b}=\frac{\rho U b}{\mu}=\frac{(998)(1)(0.2)}{0.001}=1.996 E 5 \text { Laminar }  \tag{3}\\
\delta_{x=b}=\frac{5 b}{R e_{b}^{1 / 2}}=\frac{(5)(0.2)}{(1.996 E 5)^{1 / 2}}=0.00224 \mathrm{~m}  \tag{1}\\
\left.\eta=y\left(\frac{\rho U}{\mu x}\right)^{1 / 2}=0.001\left(\frac{(1)}{(0.001)(1)}\right)^{1 / 2}\right)^{1 / 2}=2.2 \tag{1}
\end{gather*}
$$

From the table:

$$
\begin{equation*}
\frac{u}{U}=0.68132 \rightarrow u=0.68132 U=0.68132 \mathrm{~m} / \mathrm{s} \tag{1}
\end{equation*}
$$

(b)

$$
\begin{gather*}
R e_{x=L}=\frac{\rho U L}{\mu}=\frac{(998)(1)(0.4)}{0.001}=3.992 E 5 \text { Laminar }  \tag{1}\\
c_{f_{x=L}}=\frac{0.664}{R e_{x}^{1 / 2}}=\frac{0.664}{\sqrt{3.992 E 5}}=0.00105 \\
c_{f}=\frac{2 \tau_{w}}{\rho U^{2}} \rightarrow \tau_{w}=\frac{c_{f} \rho U^{2}}{2}=\frac{(0.00105)(998)(1)^{2}}{2}=0.524 \mathrm{~Pa}  \tag{1}\\
C_{D}=\frac{1.328}{R e_{L}^{1 / 2}}=\frac{1.328}{\sqrt{3.992 E 5}}=0.0021  \tag{1}\\
C_{D}=\frac{D}{0.5 \rho A U^{2}}
\end{gather*}
$$

Find drag force considering $\mathrm{A}=\mathrm{bL}$ and multiplying by 2 for both sides:

$$
\begin{equation*}
D=2 C_{D} \frac{1}{2} \rho \mathrm{bL} U^{2}=(0.0021)(998)(0.2)(0.4)(1)^{2}=0.168 \mathrm{~N} \tag{1}
\end{equation*}
$$

