

EXAM3 Solutions

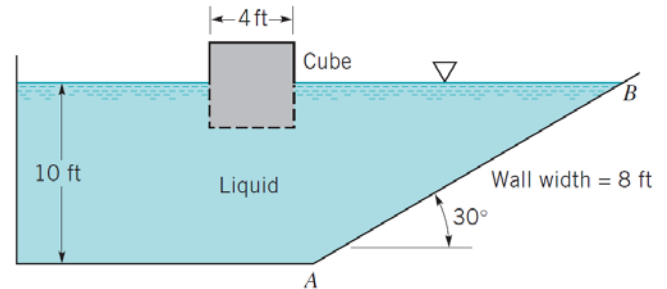
Problem 1: Hydrostatic forces on plane surfaces (Chapter 2)

Information and assumptions

- Weight of a cube : 3,000 lb
- Depth of liquid : 10 ft
- Width of the wall : 8 ft

Find

- Specific gravity fo the liquid, γ
- The force acting on the inclined section AB, F_R
- The location of the pressure center from the free surface, y_R , along the inclined wall



Solution

(a) Buoyancy force

$$W = \gamma \mathcal{V}$$

Or

$$\gamma = \frac{W}{\mathcal{V}}$$

Since \mathcal{V} is just for the immersed part only,

$$\mathcal{V} = (4 \text{ ft}) \times (4 \text{ ft}) \times (2 \text{ ft}) = 32 \text{ ft}^3$$

$$\therefore \gamma = \frac{3,000 \text{ lb}}{32 \text{ ft}^3} = \mathbf{93.75 \text{ lb/ft}^3}$$

(+3 points)

(b) Hydrostatic force

$$F_R = \bar{p} \cdot A = (\gamma h_c) \cdot A$$

$$h_c = \frac{10 \text{ ft}}{2}$$

$$A = (8 \text{ ft}) \times \left(\frac{10 \text{ ft}}{\sin 30^\circ} \right) = 160 \text{ ft}^2$$

$$\therefore F_R = \left(93.75 \frac{\text{lb}}{\text{ft}^3} \right) \left(\frac{10 \text{ ft}}{2} \right) (160 \text{ ft}^2) = \mathbf{75,000 \text{ lb}}$$

(+4 points)

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(c) Pressure center

$$y_R = \frac{I_{xc}}{y_c A} + y_c$$

$$I_{xc} = \frac{(8 \text{ ft}) \left(\frac{10 \text{ ft}}{\sin 30^\circ} \right)^3}{12} = 5333.33 \text{ ft}^4$$

$$y_c = \frac{\left(\frac{10}{\sin 30^\circ} \right)}{2} = 10 \text{ ft}$$

$$y_R = \frac{5333.33 \text{ ft}^4}{(10 \text{ ft})(160 \text{ ft}^2)} + (10 \text{ ft}) = \mathbf{13.3 \text{ ft}}$$

(+3 points)

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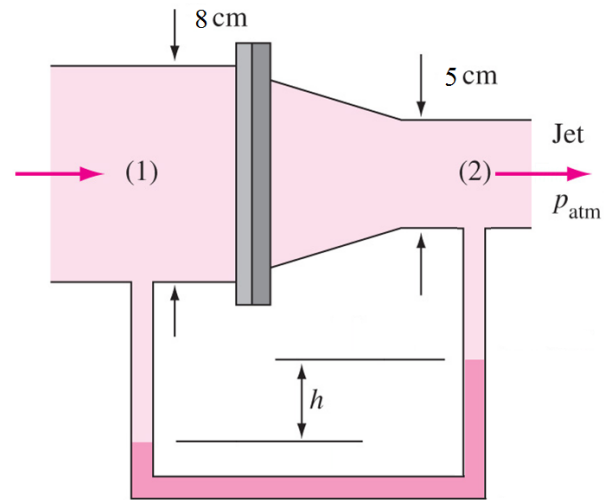
Problem 2. Linear momentum (Chap. 5)

Information and assumptions

- Water, $\gamma = 9,790 \text{ N/m}^3$
- $SG = 13.56$ for the manometer fluid
- Manometer reading, $h = 58 \text{ cm}$
- Friction is neglected.

Find

- The upstream pressure at section 1
- The average velocity at sections 1 and 2
- The axial flange force, F_x , required to keep the nozzle attached to pipe 1



Solution

(a) Manometer equation

$$p_1 - p_2 = (\gamma_m - \gamma)h = (SG - 1)\gamma h$$

where $p_2 = p_{atm} = 0$ (gage).

$$\therefore p_1 = (13.56 - 1)(9,790 \text{ N/m}^3)(0.58 \text{ m}) = \mathbf{71,300 \text{ Pa (gage)}}$$

(+2 points)

(b) Bernoulli equation

$$\frac{p_1}{\gamma} + \frac{V_1^2}{2g} + z_1 = \frac{p_2}{\gamma} + \frac{V_2^2}{2g} + z_2$$

where, $p_1 = 71,300 \text{ Pa (gage)}$, $p_2 = 0$ (gage), $V_2 = V_1 A_1/A_2 = V_1 (D_1/D_2)^2$, and $z_1 = z_2$. Thus,

$$\frac{p_1}{\gamma} + \frac{V_1^2}{2g} = \frac{\left(V_1 \left(\frac{D_1}{D_2}\right)^2\right)^2}{2g}$$

Solve for V_1 ,

$$V_1 = \sqrt{\frac{2p_1}{\rho \left[\left(\frac{D_1}{D_2}\right)^4 - 1\right]}}$$

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$$\therefore V_1 = \sqrt{\frac{(2)(71,300 \text{ Pa})}{(999 \text{ kg/m}^3) \left[\left(\frac{0.08 \text{ m}}{0.05 \text{ m}} \right)^4 - 1 \right]}} = \mathbf{5.1 \text{ m/s}}$$

From the Continuity equation,

$$V_2 = V_1 \left(\frac{D_1}{D_2} \right)^2 = (5.1 \text{ m/s}) \left(\frac{0.08 \text{ m}}{0.05 \text{ m}} \right)^2 = \mathbf{13.1 \text{ m/s}}$$

(+4 points)

(c) Momentum equation

$$p_1 A_1 - p_2 A_2 + F_x = \dot{m}(V_2 - V_1)$$

where $p_2 = 0$ (gage) and $\dot{m} = \rho V_1 A_1 = \rho V_2 A_2$. Thus

$$F_x = \rho V_1 A_1 (V_2 - V_1) - p_1 A_1$$

or

$$F_x = \left(999 \frac{\text{kg}}{\text{m}^3} \right) \left(5.1 \frac{\text{m}}{\text{s}} \right) \left(\frac{\pi}{4} \right) (0.08 \text{ m})^2 \left(13.1 \frac{\text{m}}{\text{s}} - 5.1 \frac{\text{m}}{\text{s}} \right) - (71,300 \text{ Pa}) \left(\frac{\pi}{4} \right) (0.08 \text{ m})^2 \approx \mathbf{-154 \text{ N}}$$

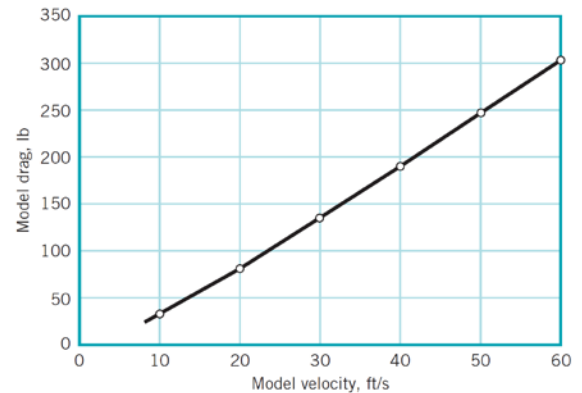
(+4 points)

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Problem 3. Similarity and model testing (Chap. 7)

Information and assumptions

- Wind velocity, $V = 44$ ft/s
- Prototype length, $L = 30$ ft
- Prototype diameter, $d = 1.25$ ft
- Air density, $\rho = 2.38 \times 10^{-3}$ slugs/ft³
- Air viscosity, $\mu = 3.74 \times 10^{-7}$ lb · s/ft²
- Model length, $L_m = 2$ ft
- Model diameter, $d_m = 1$ in.
- Water density, $\rho_m = 1.94$ slugs/ft³
- Water viscosity, $\mu_m = 2.34 \times 10^{-5}$ lb · s/ft²



Find

- Re similarity requirement
- Prediction of drag

Solution

Similarity requirements:

$$\frac{\rho_m V_m d_m}{\mu_m} = \frac{\rho V d}{\mu} \quad (\text{Re similarity})$$

$$\frac{D}{\rho V^2 d^2} = \frac{D_m}{\rho_m V_m^2 d_m^2} \quad (\text{Prediction equation})$$

(+6 points)

From the *Re* similarity requirement

$$V_m = \left(\frac{\rho}{\rho_m}\right) \left(\frac{d}{d_m}\right) \left(\frac{\mu_m}{\mu}\right) V$$

Thus, the model velocity corresponding to the full-size velocity, $V = 44$ ft/s, is

$$V_m = \left(\frac{2.38 \times 10^{-3} \frac{\text{slugs}}{\text{ft}^3}}{1.94 \frac{\text{slugs}}{\text{ft}^3}}\right) \left(\frac{1.25 \text{ ft}}{1/12 \text{ ft}}\right) \left(\frac{2.34 \times 10^{-5} \frac{\text{lb} \cdot \text{s}}{\text{ft}^2}}{3.74 \times 10^{-7} \frac{\text{lb} \cdot \text{s}}{\text{ft}^2}}\right) \left(44 \frac{\text{ft}}{\text{s}}\right) = 50.7 \frac{\text{ft}}{\text{s}}$$

(+2 points)

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From the prediction equation

$$D = \left(\frac{\rho}{\rho_m} \right) \left(\frac{V}{V_m} \right)^2 \left(\frac{d}{d_m} \right)^2 D_m$$

For $D_m = 250$ lb at $V_m = 50.7$ ft/s,

$$D = \left(\frac{2.38 \times 10^{-3} \frac{\text{slugs}}{\text{ft}^3}}{1.94 \frac{\text{slugs}}{\text{ft}^3}} \right) \left(\frac{44 \frac{\text{ft}}{\text{s}}}{50.7 \frac{\text{ft}}{\text{s}}} \right)^2 \left(\frac{1.5 \text{ ft}}{1/12 \text{ ft}} \right)^2 (250 \text{ lb}) = \mathbf{52 \text{ lb}}$$

(+2 points)

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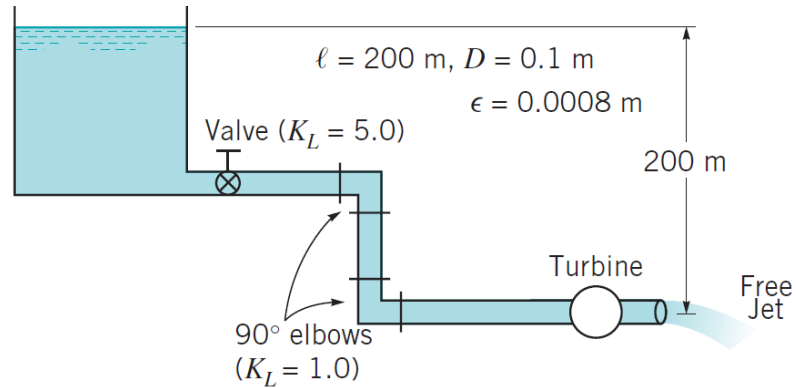
Problem 4. Major and minor loss (Chapt. 8)

Information and assumptions

- Water density, $\rho = 999 \text{ kg/m}^3$
- Viscosity, $\mu = 1.12 \times 10^{-3} \text{ N}\cdot\text{s/m}^2$
- $h_t = 116 \text{ m}$
- Entrance effects are negligible

Find

- Determine the flow rate, Q



Solution

Energy equation:

$$\frac{p_1}{\gamma} + \alpha_1 \frac{V_1^2}{2g} + z_1 = \frac{p_2}{\gamma} + \alpha_2 \frac{V_2^2}{2g} + z_2 + h_t + h_L$$

where, $p_1 = p_2 = 0(\text{gage})$, $V_1 \approx 0$, $V_2 = V$, $z_1 - z_2 = 200 \text{ m}$, $h_t = 116 \text{ m}$, $h_L = h_f + h_m$, and assume a turbulent flow thus $\alpha_2 = 1$

(+3 points)

1) Major loss:

$$h_L = f \frac{\ell}{D} \frac{V^2}{2g}$$

where, $\ell = 200 \text{ m}$ and $D = 0.1 \text{ m}$.

(+2 points)

2) Minor loss:

$$h_m = \sum K_L \frac{V^2}{2g}$$

where, $\sum K_L = 5 + 1 + 1 = 7$.

(+2 points)

Thus, the energy equation becomes

$$0 + 0 + (200 \text{ m}) = 0 + \frac{V^2}{2 \times 9.81 \text{ m/s}^2} + (116 \text{ m}) + \left(f \times \frac{200 \text{ m}}{0.1 \text{ m}} + 7 \right) \frac{V^2}{2 \times 9.81 \text{ m/s}^2}$$

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or

$$V = \left(\frac{1648}{2000f + 8} \right)^{\frac{1}{2}}$$

Assume $f = 0.02 \rightarrow V = 5.86 \rightarrow Re = 5.23 \times 10^5 \rightarrow f_{new} = 0.036 (\neq 0.02)$

Assume $f = 0.036 \rightarrow V = 4.54 \rightarrow Re = 4.05 \times 10^5 \rightarrow f_{new} = 0.0360 (= 0.036; \text{converged})$

Thus, $f = 0.036$ and $V = 4.54$ m/s.

(+2 points)

$$\therefore Q = VA = \left(4.54 \frac{\text{m}}{\text{s}} \right) \left(\frac{\pi}{4} \right) (0.1 \text{ m})^2 = \mathbf{0.0357 \text{ m}^3/\text{s}}$$

(+1 point)

Note: $Re = \frac{VD}{\nu} = \frac{\left(4.54 \frac{\text{m}}{\text{s}} \right) (0.1 \text{ m})}{1.12 \times 10^{-6}} = 4.05 \times 10^5$; a turbulent flow thus $\alpha_2 = 1$.

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Problem 5. Boundary layer (Chapt. 9)

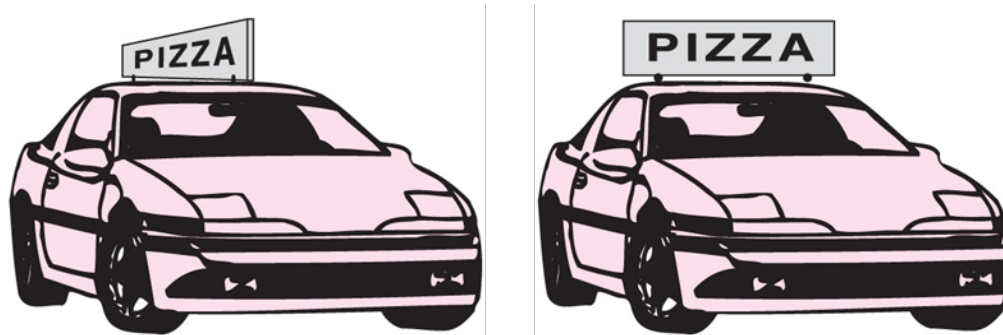
Information and assumptions

- Plate dimension: Height $H = 1.5$ ft and length $L = 5$ ft
- Incoming flow velocity, $V = 40$ mph (58.7 ft/s)
- Flow is assumed initially laminar for the parallel orientation case
- For the blunt case, drag coefficient $C_D = 1.2$

Find

- Calculate the drag D (in lbf) for both plate orientations

Solution



(a) Parallel orientation:

$$Re_L = \frac{\rho VL}{\mu} = \frac{(2.38 \times 10^{-3} \text{ slugs/ft}^3)(58.7 \text{ ft/s})(5 \text{ ft})}{3.74 \times 10^{-7} \text{ lb} \cdot \text{s/ft}^2} = 1.87 \times 10^6$$

Thus, the flow is transitional.

(+2 points)

$$C_f = \frac{0.031}{Re_L^{\frac{1}{7}}} - \frac{1440}{Re_L} = \frac{0.031}{(1.87 \times 10^6)^{\frac{1}{7}}} - \frac{1440}{1.87 \times 10^6} = 0.0032$$

(+3 points)

Thus,

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$$D = C_f \times \frac{1}{2} \rho V^2 A \times (2 \text{ sides})$$

or

$$D = (0.0032) \left(\frac{1}{2}\right) \left(2.38 \times 10^{-3} \frac{\text{slugs}}{\text{ft}^3}\right) \left(58.7 \frac{\text{ft}}{\text{s}}\right)^2 (1.5 \text{ ft} \times 5 \text{ ft} \times 2) = \mathbf{0.2 \text{ lbf}}$$

(+3 points)

(b) Normal orientation:

$$D = C_D \times \frac{1}{2} \rho V^2 A$$

or

$$D = (1.2) \left(\frac{1}{2}\right) \left(2.38 \times 10^{-3} \frac{\text{slugs}}{\text{ft}^3}\right) \left(58.7 \frac{\text{ft}}{\text{s}}\right)^2 (1.5 \text{ ft} \times 5 \text{ ft}) = \mathbf{36.9 \text{ lbf}}$$

(+2 points)

Equivalent solution 1):

$$C_f = \frac{0.074}{Re_L^{\frac{1}{5}}} - \frac{1700}{Re_L} = 0.0032$$

$$D = 0.2 \text{ lbf}$$

Equivalent solution 2):

$$C_f = \frac{0.455}{(\log Re_L)^{2.58}} - \frac{1700}{Re_L} = 0.0031$$

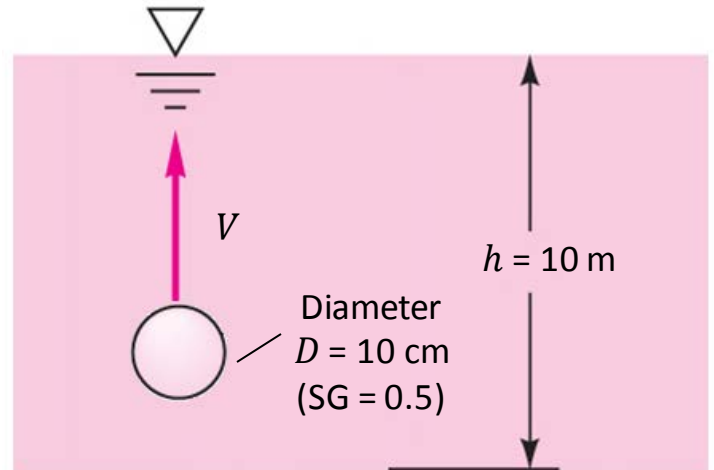
$$D = 0.2 \text{ lbf}$$

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Problem 6. Bluff body drag (Chapt. 9)

Information and assumptions

- SG of buoyant ball, $SG=0.5$
- Diameter of the ball $D=10$ cm
- Water depth $h=10$ m
- Drag coefficient $C_D = 0.5$
- The ball rises up with terminal velocity.
- Density of water, $\rho = 999$ kg/m³
- Viscosity of water, $\mu = 1.12 \times 10^{-3}$ N.s/m²
- Volume of sphere, $V = \pi D^3/6$



Find

- Time the ball takes to reach to the water surface.

Solution

(a) Rising (terminal) velocity

From a vertical force balance about the ball, Buoyancy = Weight + Drag;

$$\gamma V = \gamma_{ball} \cdot V + C_D \times \frac{1}{2} \rho V^2 A$$

(+5 points)

or

$$\gamma \cdot \frac{\pi D^3}{6} = (SG \cdot \gamma) \cdot \frac{\pi D^3}{6} + C_D \times \frac{1}{2} \rho V^2 \cdot \frac{\pi}{4} D^2$$

Solving for V ,

$$V = \sqrt{\frac{4(1 - SG)gD}{3C_D}}$$

or

$$V = \sqrt{\frac{(4)(1 - 0.5)(9.81 \text{ m/s}^2)(0.1\text{m})}{(3)(0.5)}} = 1.14 \text{ m/s}$$

(+4 points)

(b) Rising time

$$t = \frac{h}{V} = \frac{10 \text{ m}}{1.14 \text{ m/s}} \approx 9 \text{ s}$$

(+1 point)