

## EXAM2 Solutions

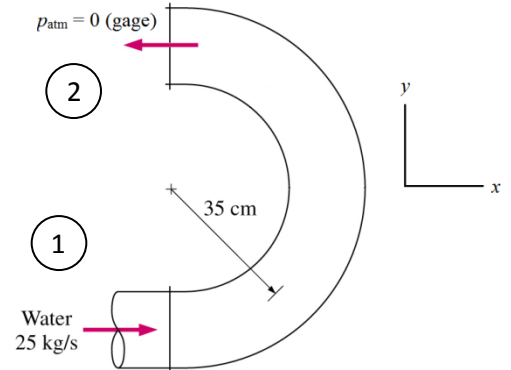
### Problem 1: Momentum equation (Chapter 5)

#### Information and assumptions

- $\rho = 1000 \text{ kg/m}^3$
- $\dot{m} = 25 \text{ kg/s}$
- $A = 10 \text{ cm}^2$
- $z_2 - z_1 = 70 \text{ cm}$
- Frictionless flow
- Weight of water and pipe is negligible
- Pressure at section (2),  $p_2 = 0$

#### Find

- Determine inlet and outlet velocities  $V_1$  and  $V_2$
- Determine gage pressure at the inlet  $p_1$
- The horizontal component of the anchoring force,  $F_x$



#### Solution

(a) Continuity:

$$\dot{m}_1 = \dot{m}_2$$

Where  $\dot{m} = V\rho A$

Therefore

$$V_1 = V_2 = V$$

Solving for  $V$

$$V = \frac{\dot{m}}{\rho A}$$

(+2.5 point)

$$V = \frac{25}{(1000) \left( \frac{\pi(0.1)^2}{4} \right)} = 3.18 \text{ m/s}$$

(+0.5 point)

(b) Bernoulli equation:

$$p_1 + \frac{1}{2}\rho V_1^2 + \gamma z_1 = p_2 + \frac{1}{2}\rho V_2^2 + \gamma z_2$$

where,  $p_2 = 0$ ,  $V_1 = V_2$ , and  $z_2 - z_1 = 0.7 \text{ m}$ , thus

$$p_1 = \gamma(z_2 - z_1)$$

(+2.5 point)

$$p_1 = (1000)(9.81)(0.7) = 6867 \text{ Pa}$$

(+0.5 point)

**EXAM2 Solutions**(c)  $x$ -momentum:

$$F_x + p_1 A_1 = \dot{m}(-V_2) - \dot{m}(V_1) = -2\dot{m}V$$

or

$$F_x = -2\dot{m}V - p_1 A_1$$

**(+3.5 points)**

$$F_x = -(2)(25)(3.18) - (6867) \left( \frac{\pi(0.1)^2}{4} \right) = -213 \text{ N}$$

**(+0.5 point)**

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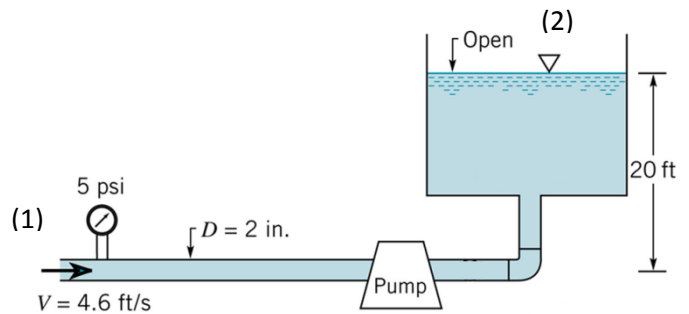
### Problem 2: Energy equation (Chapter 5)

#### Information and assumptions

- Oil,  $\gamma = 48.0 \text{ lb/ft}^3$ ,  $\mu = 2.0 \times 10^{-5} \text{ lb}\cdot\text{s/ft}^2$
- Head loss  $h_L = 41.3 \bar{V}^2/2g$
- Flow rate  $Q = 1,600 \text{ gal/min}$
- kinetic energy correction factor  $\alpha$  is 1
- $1 \text{ hp} = 550 \text{ ft}\cdot\text{lb/s}$

#### Find

- Pump power  $\dot{W}_p$



#### Solution

Energy equation

$$\frac{p_1}{\gamma} + \frac{V_1^2}{2g} + z_1 + h_p = \frac{p_2}{\gamma} + \frac{V_2^2}{2g} + z_2 + h_t + h_L$$

Where,  $z_1 - z_2 = 20 \text{ ft}$ ,  $p_2 = 0$ ,  $V_2 = 0$ ,  $h_t = 0$ .

$$h_p = -\frac{p_1}{\gamma} - \frac{V_1^2}{2g} + (z_2 - z_1) + 41.3 \frac{\bar{V}^2}{2g}$$

(+6.5 points)

$$h_p = -\frac{(5)(144)}{48} - \frac{(4.6)^2}{(2)(32.2)} + 20 + 41.3 \frac{(4.6)^2}{(2)(32.2)} = 18.24 \text{ ft}$$

(+0.5 points)

Thus,

$$\dot{W}_p = \gamma Q h_p = \gamma (VA) h_p$$

(+2.5 points)

$$\dot{W}_p = (48)(4.6) \frac{(\pi)(2/12)^2}{4} (18.24) = 87.86 \frac{\text{ft}\cdot\text{lb}}{\text{s}} = 0.16 \text{ hp}$$

(+0.5 point)

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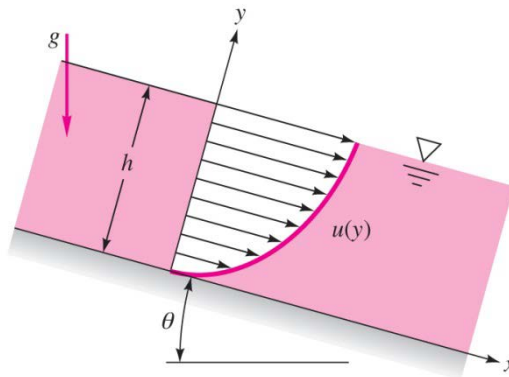
### Problem 3: Exact solution of NS equation (Chapter 6)

#### Information and assumptions

- Pressure gradient in x-direction,  $\frac{\partial p}{\partial x} = 0$
- Steady, fully-developed, one dimensional and laminar

#### Find

- Velocity profile function  $u(y)$
- If the liquid is SAE 30W oil ( $\rho = 891 \text{ kg/m}^3$  and  $\mu = 0.28 \text{ kg/m}\cdot\text{s}$ ),  $h = 10 \text{ mm}$ , and  $\theta = 30^\circ$ , determine the flow rate per unit width (into the paper)



#### Solution

(a) Navier-Stokes equation:

$$\rho \left( \underbrace{\frac{\partial u}{\partial t}}_{\substack{=0 \\ \text{steady}}} + \underbrace{u \frac{\partial u}{\partial x}}_{\substack{=0 \\ \text{continuity}}} + \underbrace{v \frac{\partial u}{\partial y}}_{=0} + \underbrace{w \frac{\partial u}{\partial z}}_{=0} \right) = - \underbrace{\frac{\partial p}{\partial x}}_{=0} + \rho g_x + \mu \left( \underbrace{\frac{\partial^2 u}{\partial x^2}}_{=0} + \frac{\partial^2 u}{\partial y^2} + \underbrace{\frac{\partial^2 u}{\partial z^2}}_{\substack{\text{infinite} \\ \text{plate}}} \right)$$

Thus,

$$0 + u \times 0 + 0 \times \frac{\partial u}{\partial y} + 0 \times \frac{\partial u}{\partial z} = -0 + \rho g \sin \theta + \mu \frac{\partial^2 u}{\partial y^2}$$

or

$$\frac{d^2 u}{dy^2} = -\frac{\rho g}{\mu} \sin \theta$$

Integration yields,

$$\frac{du}{dy} = -\frac{\rho g}{\mu} \sin \theta y + C_1$$

and

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$$u = -\frac{\rho g}{\mu} \sin \theta \frac{y^2}{2} + C_1 y + C_2$$

B.C.

$$u = 0 \text{ at } y = 0,$$

$$0 = 0 + 0 + C_2$$

$$\frac{du}{dy} = 0 \text{ at } y = h,$$

$$0 = -\frac{\rho g}{\mu} \sin \theta h + C_1$$

Thus,

$$u = \frac{\rho g}{\mu} \sin \theta \left( hy - \frac{y^2}{2} \right)$$

**(+7 points)**

(b) Flow rate per unit width

$$q = \int_0^h \frac{\rho g}{\mu} \sin \theta \left( hy - \frac{y^2}{2} \right) dy = \frac{\rho g h^3 \sin \theta}{3\mu}$$

**(+2.5 points)**

$$q = \frac{(891)(9.81)(0.01)^3 (\sin 30^\circ)}{(3)(0.28)} = 0.0052 \text{ m}^2/\text{s}$$

**(+0.5 point)**

**EXAM2 Solutions****Problem 4: Dimensional analysis (Chapter 7)****Information and assumptions**

- $D = f(d, \rho, V)$
- $d_m = 0.3 \text{ ft}$ ,  $\gamma_m = 53 \frac{\text{lb}}{\text{ft}^3}$ ,  $V_m = 5 \text{ ft/s}$ ,  $D_m = 1.4 \text{ lb}$
- $d = 2 \text{ ft}$ ,  $\gamma = 1.94 \text{ slug/ft}^3$ ,  $V = 3 \text{ ft/s}$

**Find**

- Find dimensionless parameters.
- Find drag on the prototype.

**Solution**

(a)

$$D = f(d, \rho, V)$$

where  $D \doteq F$ ,  $d \doteq L$ ,  $\rho \doteq FL^{-4}T^2$ , and  $V \doteq LT^{-1}$

Thus  $k - r = 4 - 3 = 1$  pi term required. By choosing  $d, \rho, V$  as the repeating variables,

$$\Pi = Dd^a\rho^bV^c$$

and in terms of dimensions

$$(F)(L)^a(FL^{-4}T^2)^b(LT^{-1})^c \doteq F^0L^0T^0$$

To be dimensionless it follows that

$$\begin{aligned} F: \quad 1 + b &= 0 \\ L: \quad a - 4b + c &= 0 \\ T: \quad 2b - c &= 0 \end{aligned}$$

therefore,  $a = -2$ ,  $b = -1$ ,  $c = -2$ . The pi term then becomes

$$\frac{D}{\rho V^2 d^2} = \Pi_1 = C_D$$

**(+7 point)**

(b)

$$\frac{D}{\rho V^2 d^2} = \frac{D_m}{\rho_m V_m^2 d_m^2}$$

or

$$D = \left(\frac{\rho}{\rho_m}\right) \left(\frac{V}{V_m}\right)^2 \left(\frac{d}{d_m}\right)^2 D_m$$

**(+2.5 point)**

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$$\therefore D = \left(\frac{1.94}{53/32.2}\right) \left(\frac{3}{5}\right)^2 \left(\frac{2}{0.3}\right)^2 (1.4) = 26.4 \text{ lb}$$

**(+0.5 point)**