Information and assumptions

Provided in problem statement

Find

The differential height of mercury between the two pipe sections

Solution

Take points 1 and 2 along the centerline of the pipe over two tubes of the manometer.

$$V_{1} = \frac{Q}{A_{1}} = \frac{Q}{\frac{1}{4}\pi D_{1}^{2}} = \frac{1gal}{\frac{1}{4}\pi \left(\frac{4}{12}\right)^{2}} = \frac{0.13368 ft^{3}}{1gal} = 1.53 ft/s$$

$$V_{2} = \frac{Q}{A_{2}} = \frac{Q}{\frac{1}{4}\pi D_{2}^{2}} = \frac{1gal}{\frac{1}{4}\pi \left(\frac{2}{12}\right)^{2}} = \frac{0.13368 ft^{3}}{1gal} = 6.13 ft/s$$

$$(+2)$$

Bernoulli equation between points 1 and 2:

$$\frac{P_1}{\rho_w g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho_w g} + \frac{V_2^2}{2g} + Z_2$$

$$P_1 - P_2 = \frac{1}{2} \rho_w \left(V_2^2 - V_1^2 \right)$$
(+3)

Manometer equation

(1)

$$P_{1} + \rho_{w}g(s+h) = P_{2} + \rho_{w}gs + \rho_{Hg}gh$$
(2)
$$P_{1} - P_{2} = (\rho_{Hg} - \rho_{w})gh$$
(+3)

Combing eqn (1) and (2) and solving for h

$$h = \frac{\rho_w \left(V_2^2 - V_1^2\right)}{2g\left(\rho_{Hg} - \rho_w\right)} = \frac{\left(V_2^2 - V_1^2\right)}{2g\left(\frac{\rho_{Hg}}{\rho_w} - 1\right)}$$

$$h = \frac{\left(6.13^2 - 1.53^2\right)}{2\left(32.2 \, ft/s^2\right) \left(\frac{847}{62.4} - 1\right)} = 0.0435 \, ft = 0.522 in \tag{+2}$$

Information and assumptions

Provided in problem statement

Find

- (a) The average water exit velocity
- (b) The horizontal resistance force

Solution

The average outlet velocity

$$V = \frac{Q}{A} = \frac{Q}{\frac{1}{4}\pi D^2} = \frac{5m^3/\min}{\frac{1}{4}\pi (0.06)^2} = 1768 \, m/\min = 29.5 \, m/s$$
(+3)

The mass flow rate

$$\dot{m} = \rho Q = (1000 \, kg/m^3)(5 \, m^3/) = 5000 \, kg/\min = 83.3 \, kg/s$$
(+2)

The momentum equation for steady one-dimensional flow:

$$\sum F_R = \sum_{out} \beta \dot{m} V - \sum_{in} \beta \dot{m} V \tag{+3}$$

$$F_R = \dot{m}V_e - 0 = \dot{m}V = (83.3 \, kg/s)(29.5 \, m/s) = 2457 N$$

(+2)

Information and assumptions

Provided in problem statement

Find

The air velocity in the wind tunnel

Solution

Reynolds number similarity

$$Re_m = Re_p$$

$$\frac{V_m L_m}{V_m} = \frac{V_p L_p}{V_p}$$

(+7)

$$V_{air} = \frac{L_p}{L_m} \frac{v_m}{v_p} V_p = \frac{L_w}{L_{air}} \frac{v_{air}}{v_w} V_w$$

(+2)

$$= \left(\frac{1}{1}\right) \left(\frac{1.41 \times 10^{-5}}{1.31 \times 10^{-6}}\right) (10) = 107.6 \, m/s$$

(+1)

Information and assumptions

Provided in problem statement

Find

The head loss

Solution

The average velocity:

$$V = \frac{\dot{m}}{\rho A_c} = \frac{\dot{m}}{\rho \left(\pi D^2 / 4\right)} = \frac{0.15}{(665.1) \left(\pi 0.005^2 / 4\right)} = 11.49 \, \text{m/s}$$
(+2)

The Reynolds number:

Re =
$$\frac{\rho VD}{\mu}$$
 = $\frac{(665.1)(11.49)(0.005)}{2.361 \times 10^{-4}}$ = 1.618×10⁵

Therefore the flow is turbulent

(+2)

The relative roughness of the pipe

$$\varepsilon/D = \frac{1.5 \times 10^{-6}}{0.005} = 3 \times 10^{-4}$$

(+1)

From Moody chart: f = 0.019

(+1)

Head loss:

$$h_L = f \frac{L}{D} \frac{V^2}{2g} = 0.019 \times \frac{30}{0.005} \times \frac{11.49^2}{2(9.81)} = 767m$$

(+4)