

7.5

7.5 At a sudden contraction in a pipe the diameter changes from  $D_1$  to  $D_2$ . The pressure drop,  $\Delta p$ , which develops across the contraction is a function of  $D_1$  and  $D_2$ , as well as the velocity,  $V$ , in the larger pipe, and the fluid density,  $\rho$ , and viscosity,  $\mu$ . Use  $D_1$ ,  $V$ , and  $\mu$  as repeating variables to determine a suitable set of dimensionless parameters. Why would it be incorrect to include the velocity in the smaller pipe as an additional variable?

$$\Delta p = f(D_1, D_2, V, \rho, \mu)$$

$$\Delta p \doteq FL^{-2} \quad D_1 \doteq L \quad D_2 \doteq L \quad V \doteq LT^{-1} \quad \rho \doteq FL^{-3} \quad \mu \doteq FL^{-2}T$$

From the pi theorem,  $6 - 3 = 3$  dimensionless parameters required. Use  $D_1$ ,  $V$ , and  $\mu$  as repeating variables. Thus,

$$\pi_1 = \Delta p D_1^a V^b \mu^c$$

$$\text{and } (FL^{-2})(L)^a (LT^{-1})^b (FL^{-2}T)^c \doteq F^0 L^0 T^0$$

so that

$$1 + c = 0 \quad (\text{for } F)$$

$$-2 + a + b - 2c = 0 \quad (\text{for } L)$$

$$-b + c = 0 \quad (\text{for } T)$$

It follows that  $a=1$ ,  $b=-1$ ,  $c=-1$ , and therefore

$$\pi_1 = \frac{\Delta p D_1}{V \mu}$$

Check dimensions using MLT system:

$$\frac{\Delta p D_1}{V \mu} \doteq \frac{(ML^{-1}T^{-2})(L)}{(LT^{-1})(ML^{-1}T^{-1})} \doteq M^0 L^0 T^0 \quad \therefore \text{OK}$$

For  $\pi_2$ :

$$\pi_2 = D_2 D_1^a V^b \mu^c$$

$$L (L)^a (LT^{-1})^b (FL^{-2}T)^c \doteq F^0 L^0 T^0$$

$$c = 0 \quad (\text{for } F)$$

$$1 + a + b - 2c = 0 \quad (\text{for } L)$$

$$-b + c = 0 \quad (\text{for } T)$$

It follows that  $a=-1$ ,  $b=0$ ,  $c=0$ , and therefore

$$\pi_2 = \frac{D_2}{D_1}$$

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$\pi_2$  is obviously dimensionless.

For  $\pi_3$ :

$$\pi_3 = \rho D_1^a V^b \mu^c$$

$$(FL^{-4}T^2)(L)^a(LT^{-1})^b(FL^{-2}T)^c = F^0L^0T^0$$

$$1+c=0 \quad (\text{for } F)$$

$$-4+a+b-2c=0 \quad (\text{for } L)$$

$$2-b+c=0 \quad (\text{for } T)$$

It follows that  $a=1$ ,  $b=1$ ,  $c=-1$  and therefore

$$\pi_3 = \frac{\rho D_1 V}{\mu}$$

Check dimensions using MLT system:

$$\frac{\rho D_1 V}{\mu} = \frac{(ML^{-3})(L)(LT^{-1})}{ML^{-1}T^{-1}} = M^0L^0T^0 \quad \therefore \text{OK}$$

Thus,

$$\frac{\Delta p D_1}{V \mu} = \phi \left( \frac{D_2}{D_1}, \frac{\rho D_1 V}{\mu} \right)$$

From the continuity equation,

$$V \frac{\pi}{4} D_1^2 = V_s \frac{\pi}{4} D_2^2$$

where  $V_s$  is the velocity in the smaller pipe. Since

$$V_s = \left( \frac{D_1}{D_2} \right)^2 V$$

$V_s$  is not independent of  $D_1$ ,  $D_2$ , and  $V$  and therefore should not be included as an independent variable.